



CO₂ Foam for EOR and CO₂ Storage in CCUS

From Laboratory to Field-scale

Zachary Paul Alcorn and Arne Graue

October 18, 2022



Reservoir Physics Group Research



- Carbon capture, **utilization and storage** (CCUS)
- Hydrogen storage and production
- Gas hydrates

Fluid flow in porous media
Laboratory to field-scale



Climate change mitigation and energy security

Reservoir Physics Group Research



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CCUS, CO₂ foam
EOR, gas hydrates,
wettability



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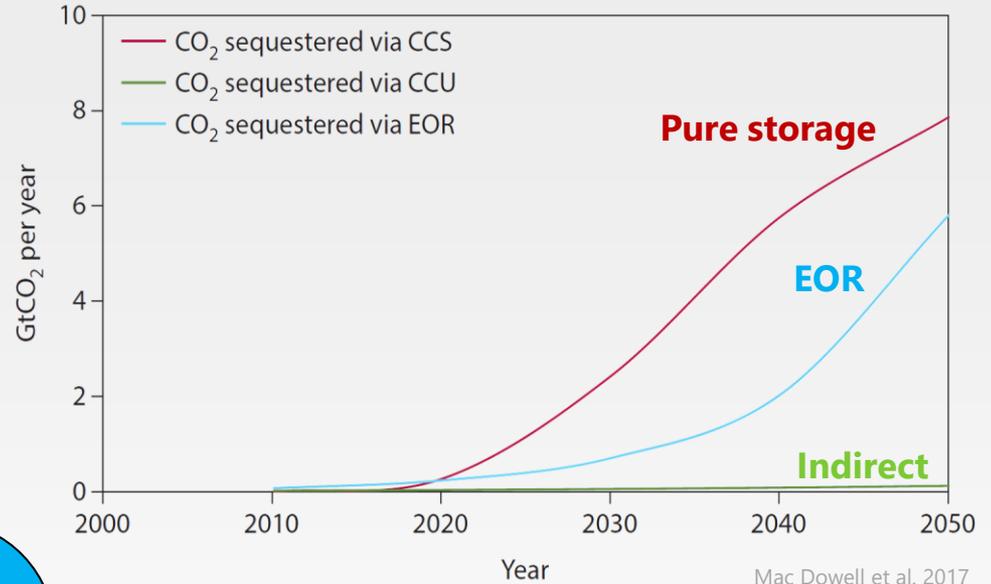
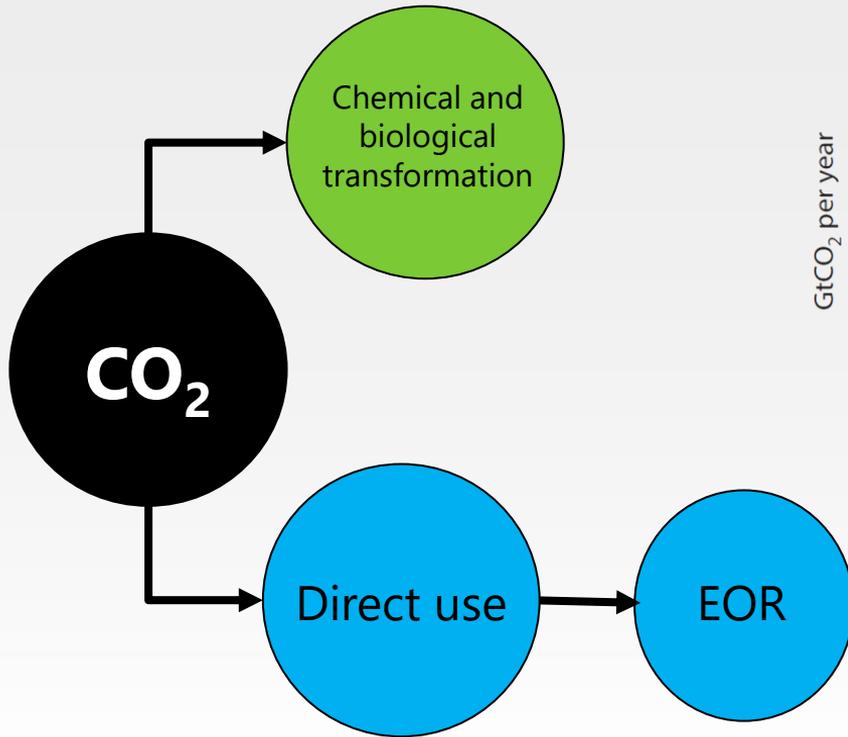
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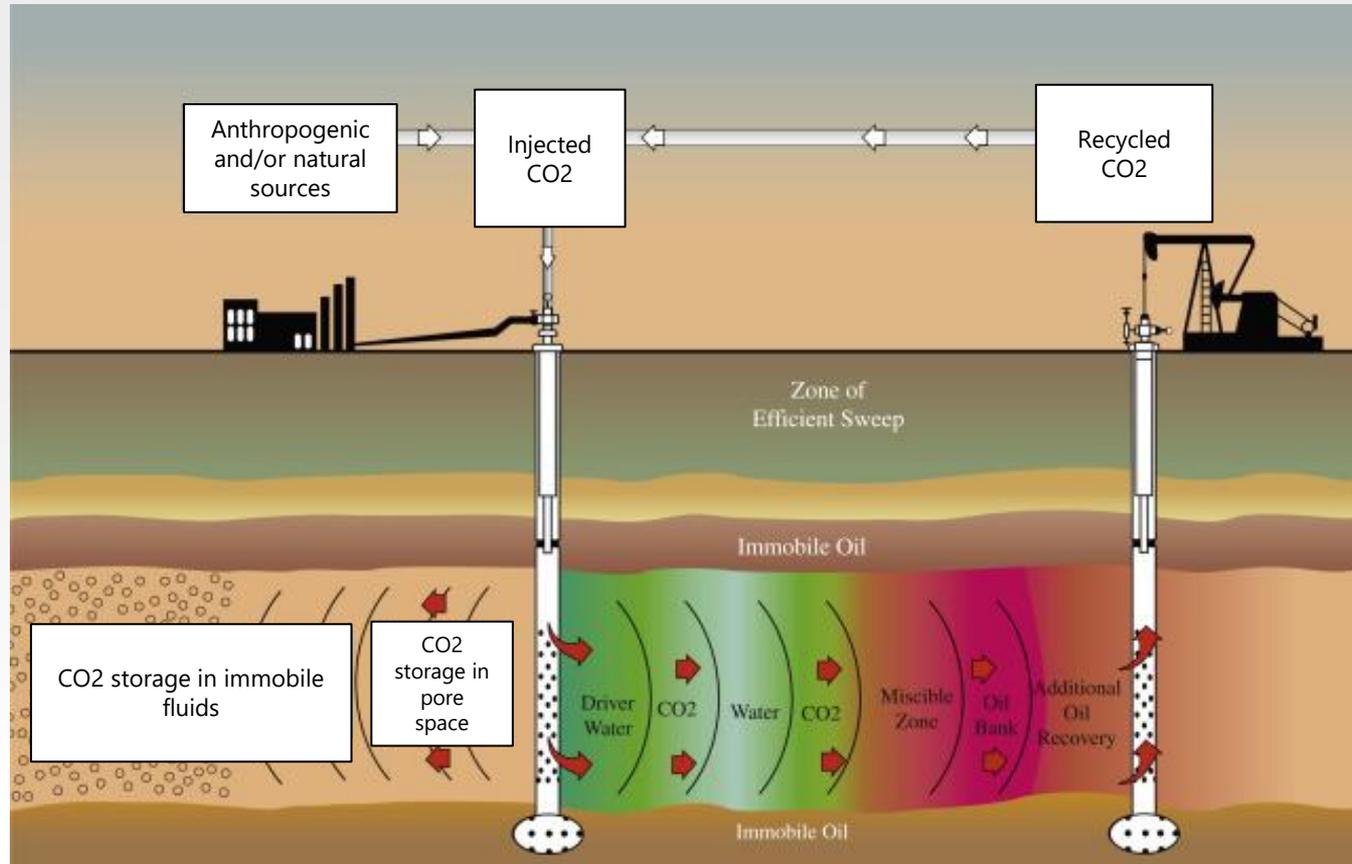
Focus areas:

CCUS, CO₂ EOR
and storage, CO₂
foam, reservoir
simulation, energy
transition

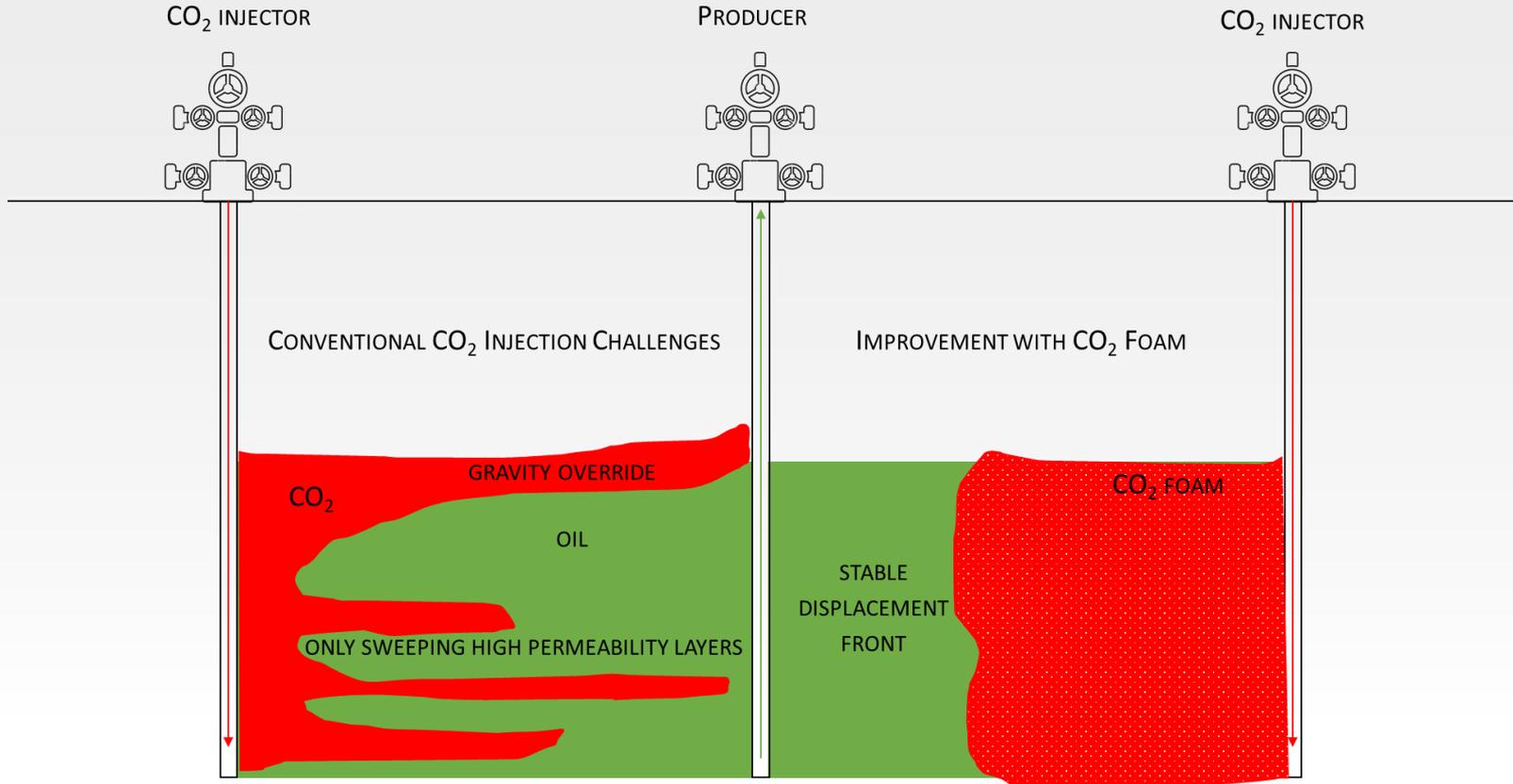
CO₂ Utilization and Storage



CO₂ Utilization and Storage

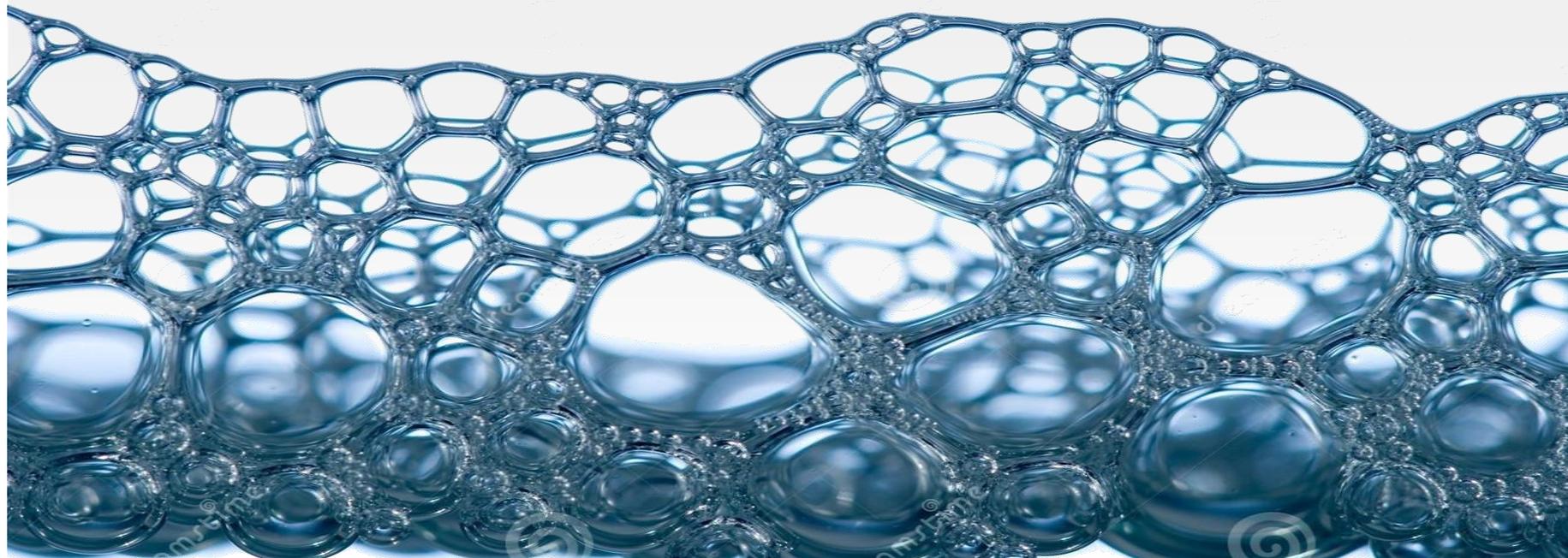


CO₂ Utilization and Storage





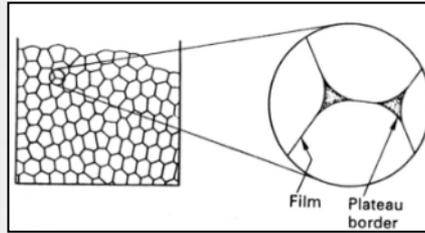
CO₂ Foam



CO₂ Foam Fundamentals

What?

- Dispersion of gas in liquid
- Stabilized by surfactant

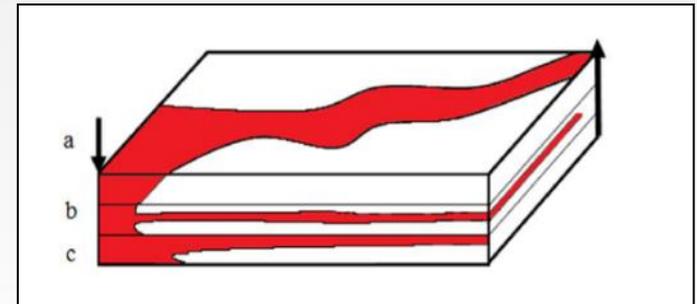
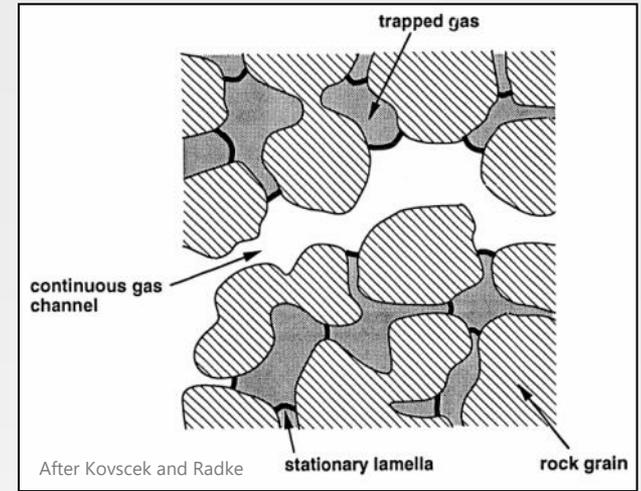


How?

- Decreases relative permeability
- Increases viscosity
- Injection strategy: SAG or co-injection

Why?

- Conformance and mobility control
- Increase reservoir sweep and displacement
- Additional CO₂ storage



Sc-CO₂ EOR mobility challenges: a) poor aerial sweep, b) gas channeling, c) gravity override (Hanssen et al., 1994)

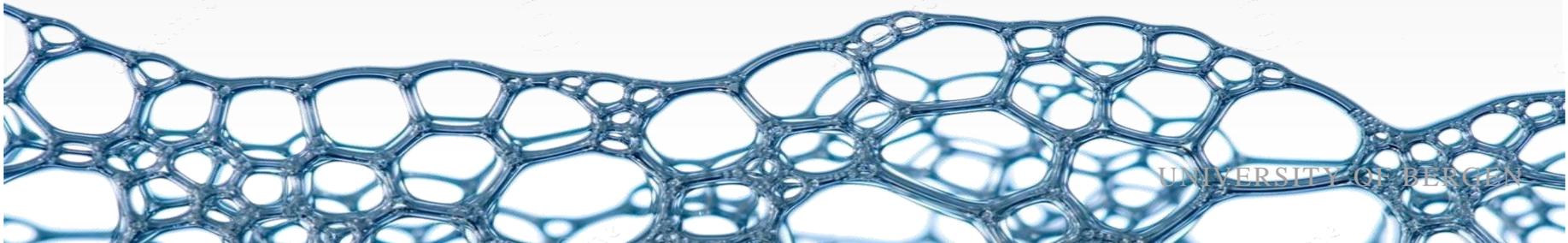
The Foam Challenge



- Complex flow behavior
- Foam mobility depends on bubble density, which changes continuously during generation and coalescence.
- Opaque core-scale systems
- Foam generation and stability are impacted by the presence of oil.



[istockphoto.com/vector/bridging-the-gap-gm966203348-263631621](https://www.istockphoto.com/vector/bridging-the-gap-gm966203348-263631621)



Laboratory Scales

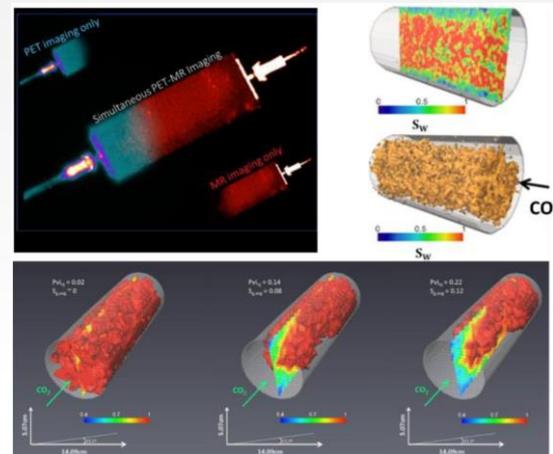
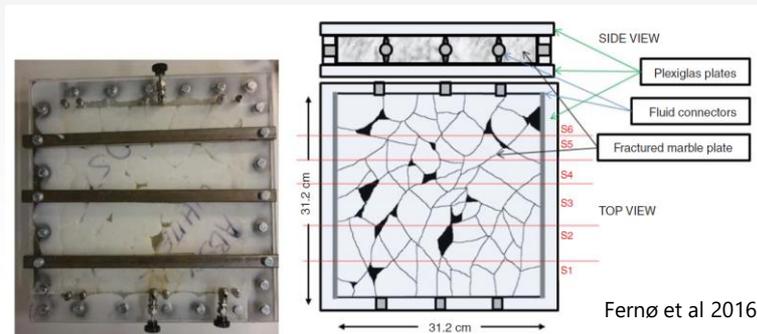
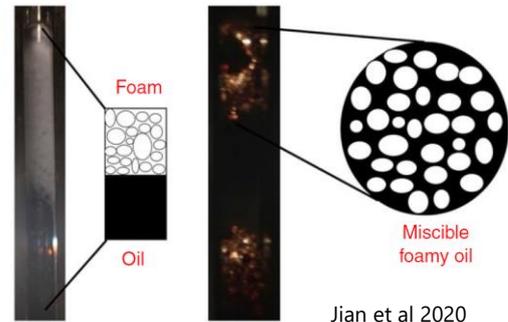
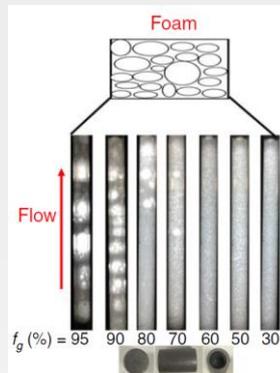
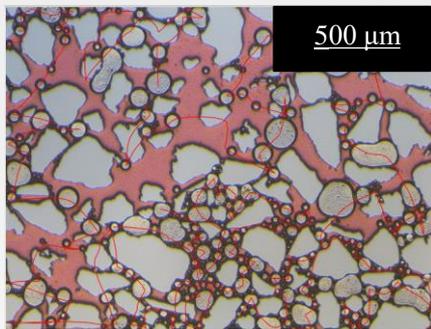


- Bulk

- Pore

- Core

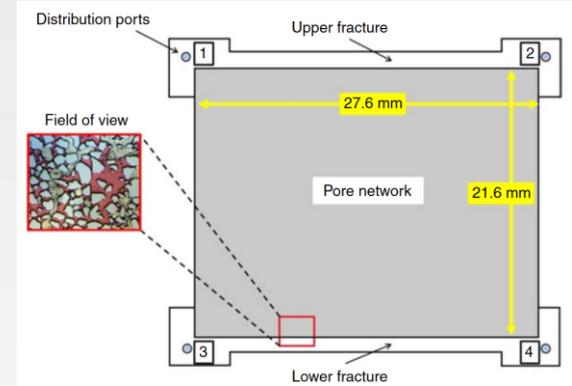
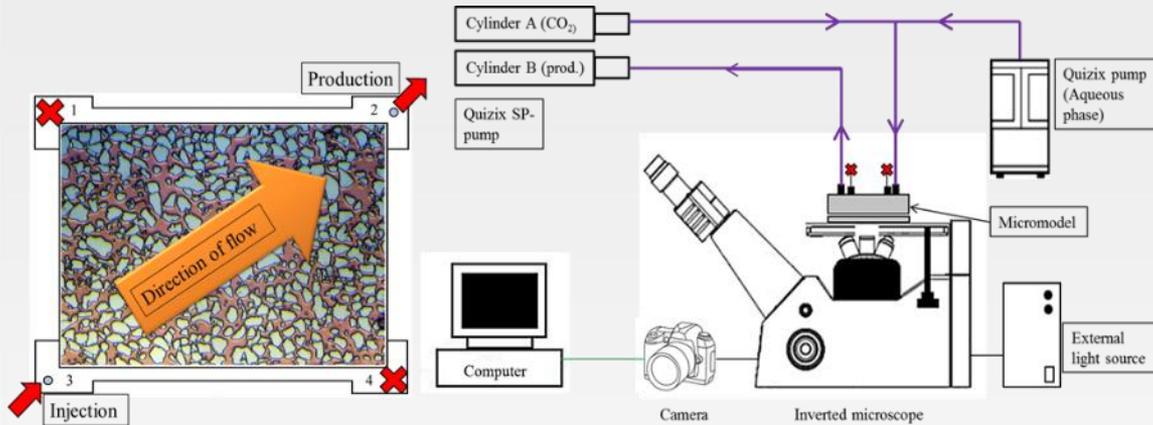
- Block





Pore-scale CO₂ Foam

Set-up and Properties

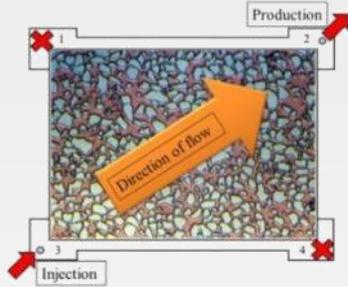


Rognmo et al. 2019

Porosity (%)	Permeability (md)	Avg. Grain Size (μm)
≈ 60	2.9	99.3

1305 psi, 20°C

Pore-Scale Baseline (no surfactant)

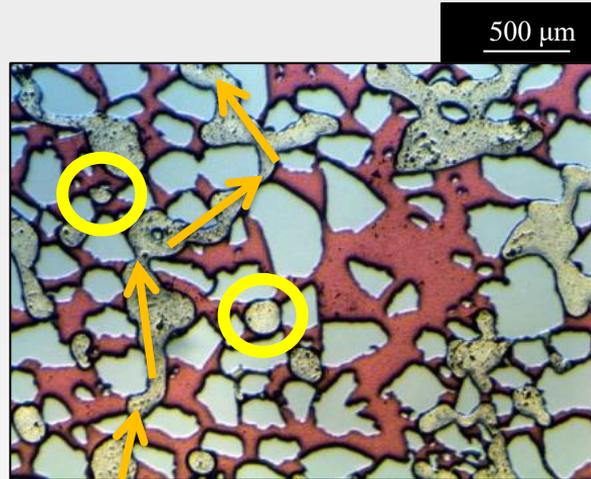


1305 psi, 20°C

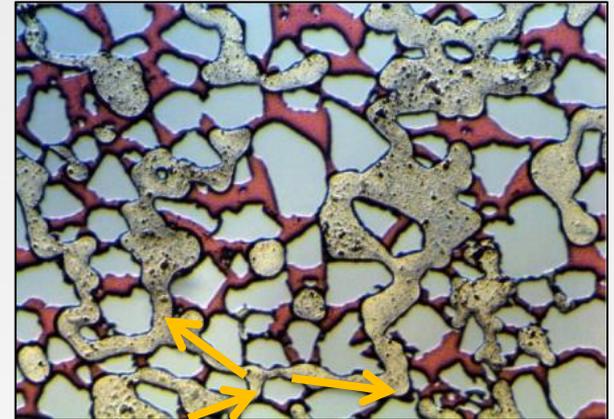
100% brine saturated

Gas fraction (f_g) = 0.70

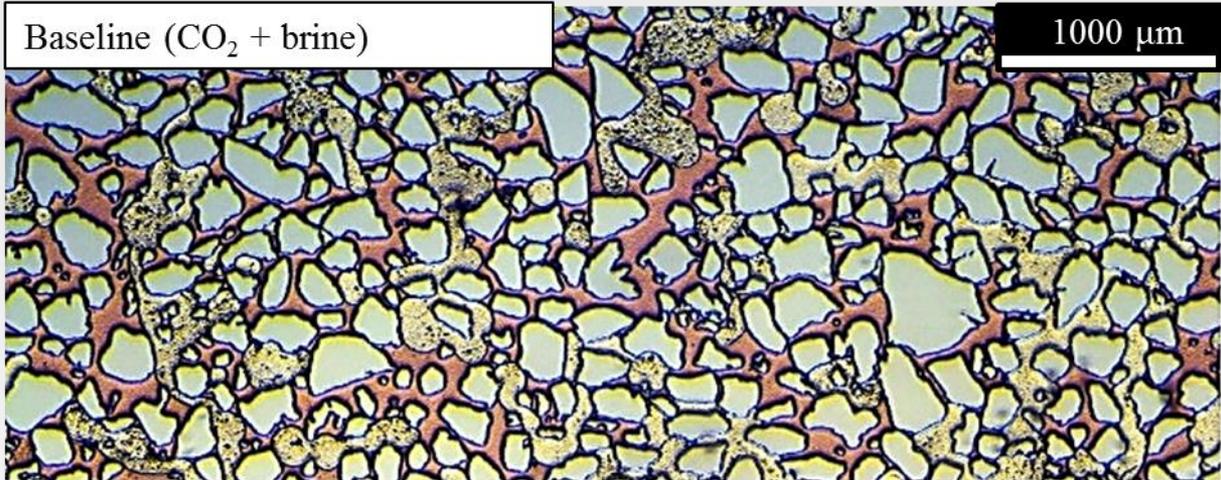
CO₂ phase spanning over several pores without being separated by liquid films, indicating low CO₂ mobility reduction



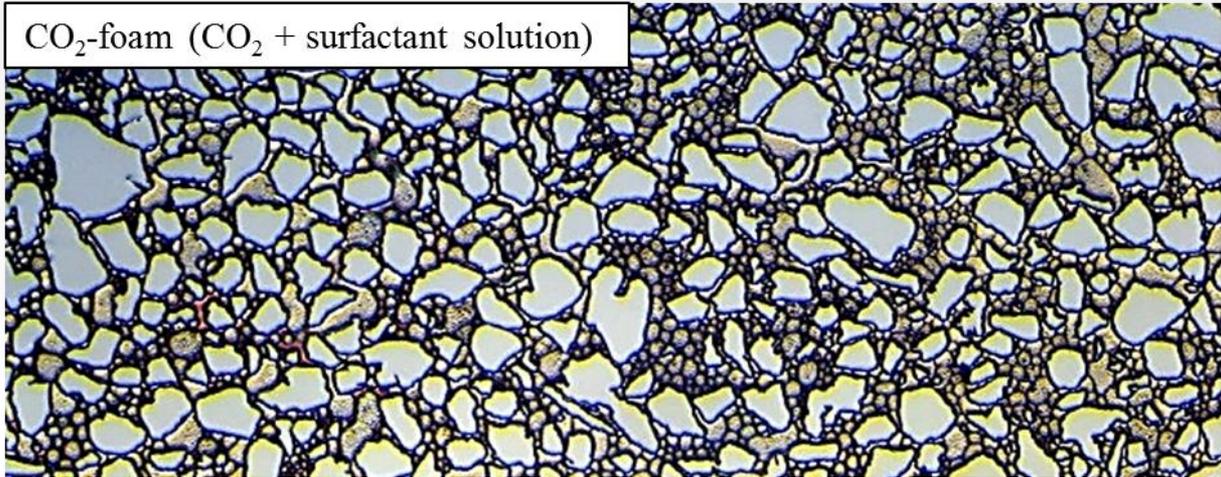
Red is water, light blue uniform areas are grains, brown textured areas are CO₂



Baseline (CO_2 + brine)



CO_2 -foam (CO_2 + surfactant solution)



Red is water, light blue uniform areas are grains, brown textured areas are CO_2

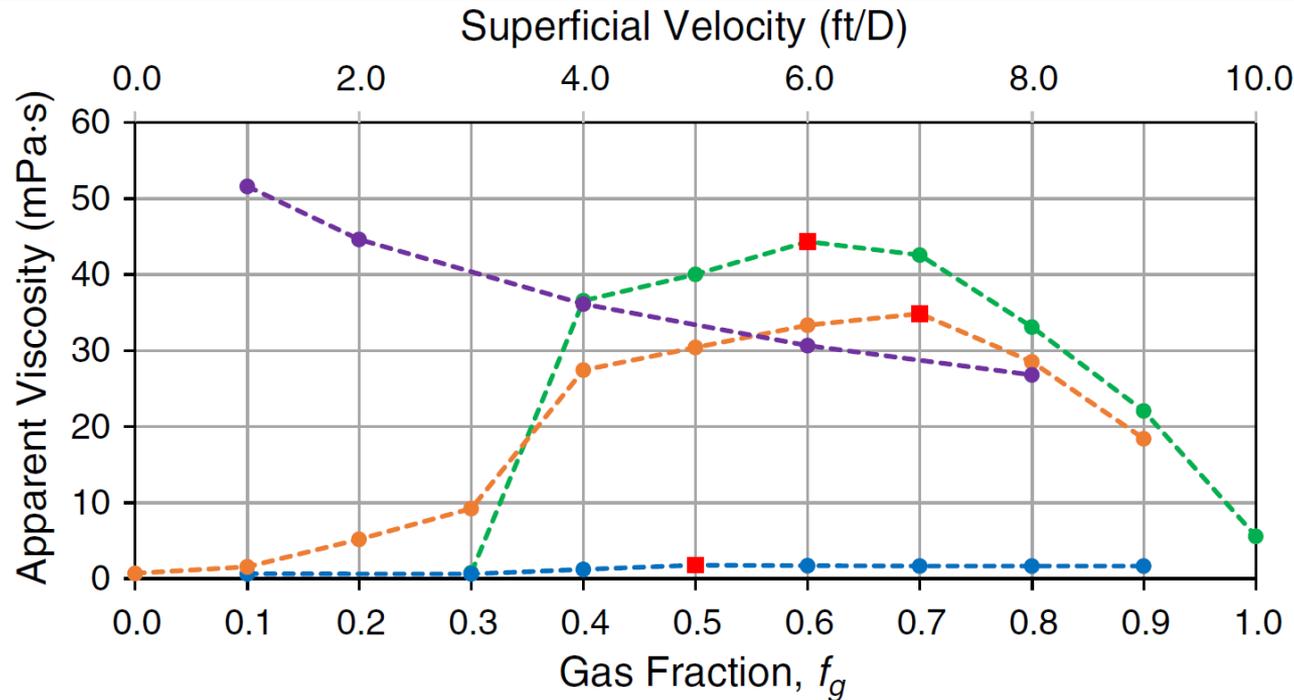




Core-scale CO₂ Foam

Steady- and unsteady-state flow

Steady-state Foam Quality and Rate Scan



2500 psi and 40C
 Injection rate: 1 ft/day
 100% brine-saturated
 1 wt% surfactant solution

- Foam-quality scan-reservoir plug
- Foam-quality scan-baseline
- Foam-quality scan-outcrop plug
- Optimal gas fractions
- Foam-rate scan-reservoir plug

Core Identity	Length (cm)	Diameter (cm)	Pore Volume (mL)	Porosity (%)	Permeability (md)
Reservoir	5.7	5.0	15.2	13.8	22.1
Outcrop	7.5	5.0	35.3	24.2	20.5

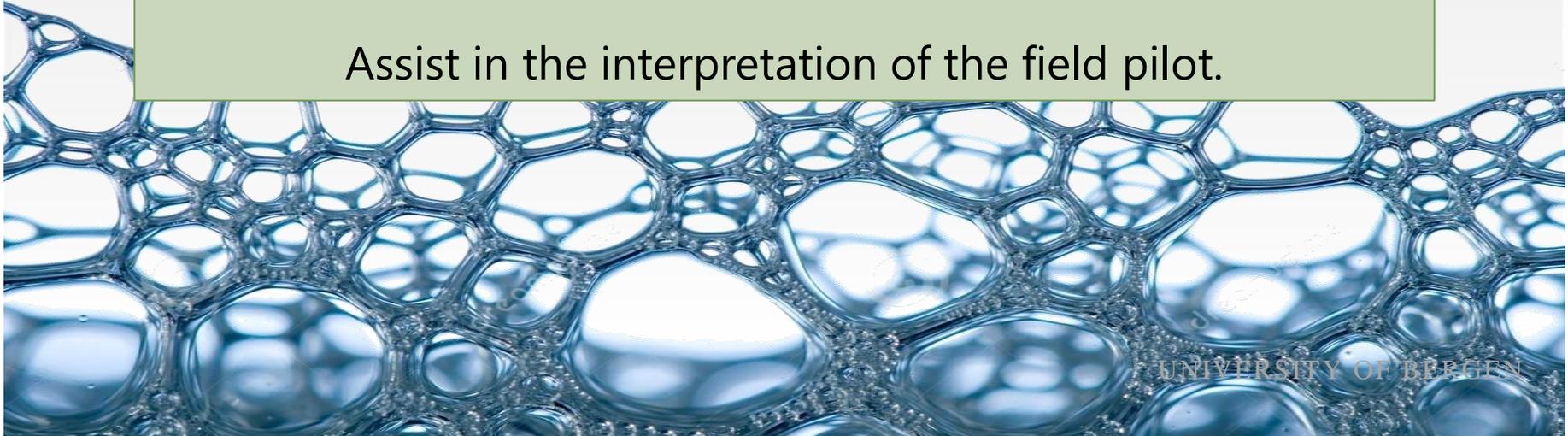


Unsteady-state

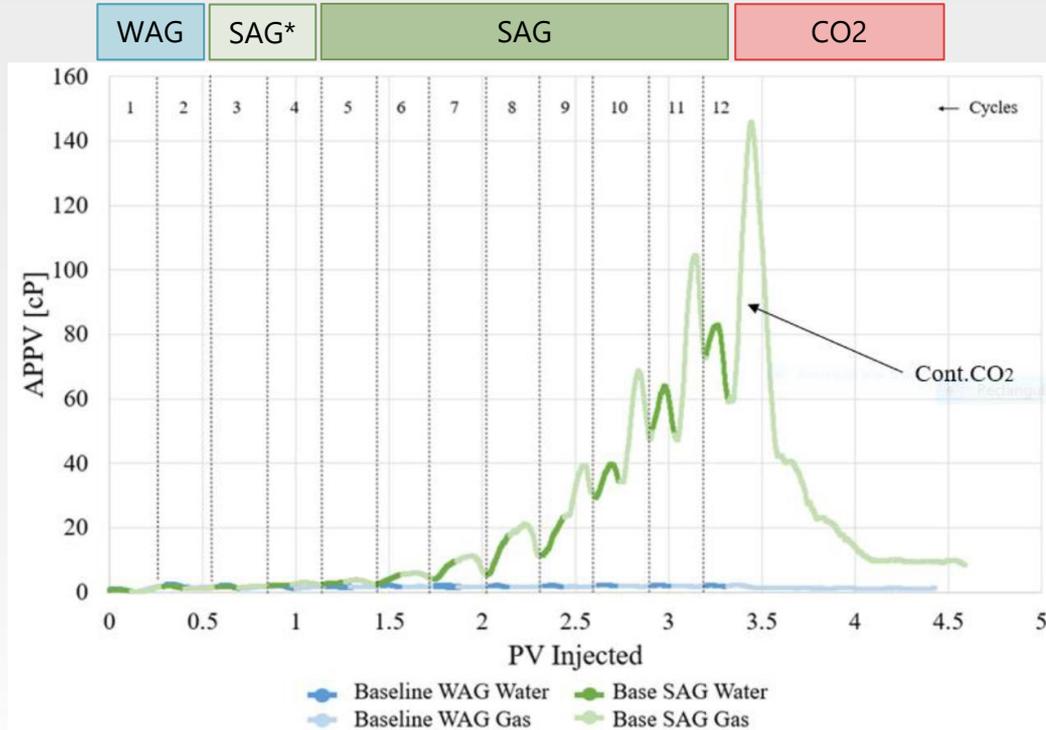
Foam generation, strength and stability during unsteady-state alternating slug injection of surfactant solution and CO₂.

Develop a methodology for evaluating CO₂ foam during unsteady-state injection.

Assist in the interpretation of the field pilot.



Unsteady-state: Baseline WAG vs SAG



2800 psi and 40C
 100% brine saturated
 0.5 wt% surfactant solution
 Injection rate: 4 ft/day
 Gas fraction: 0.60

Properties	Value
Length [cm]	24.40 ± 0.01
Diameter [cm]	3.88 ± 0.01
Permeability [D]	2.14 ± 0.03
Pore Volume [ml]	62.16 ± 0.01
Porosity [%]	21.54 ± 0.10



CO₂ Foam EOR and CO₂ Storage



Evaluate EOR and CO₂ storage potential of CO₂ foam systems

- water-soluble nonionic Surfonic L24-22 (0.5 wt% and 1 wt%)

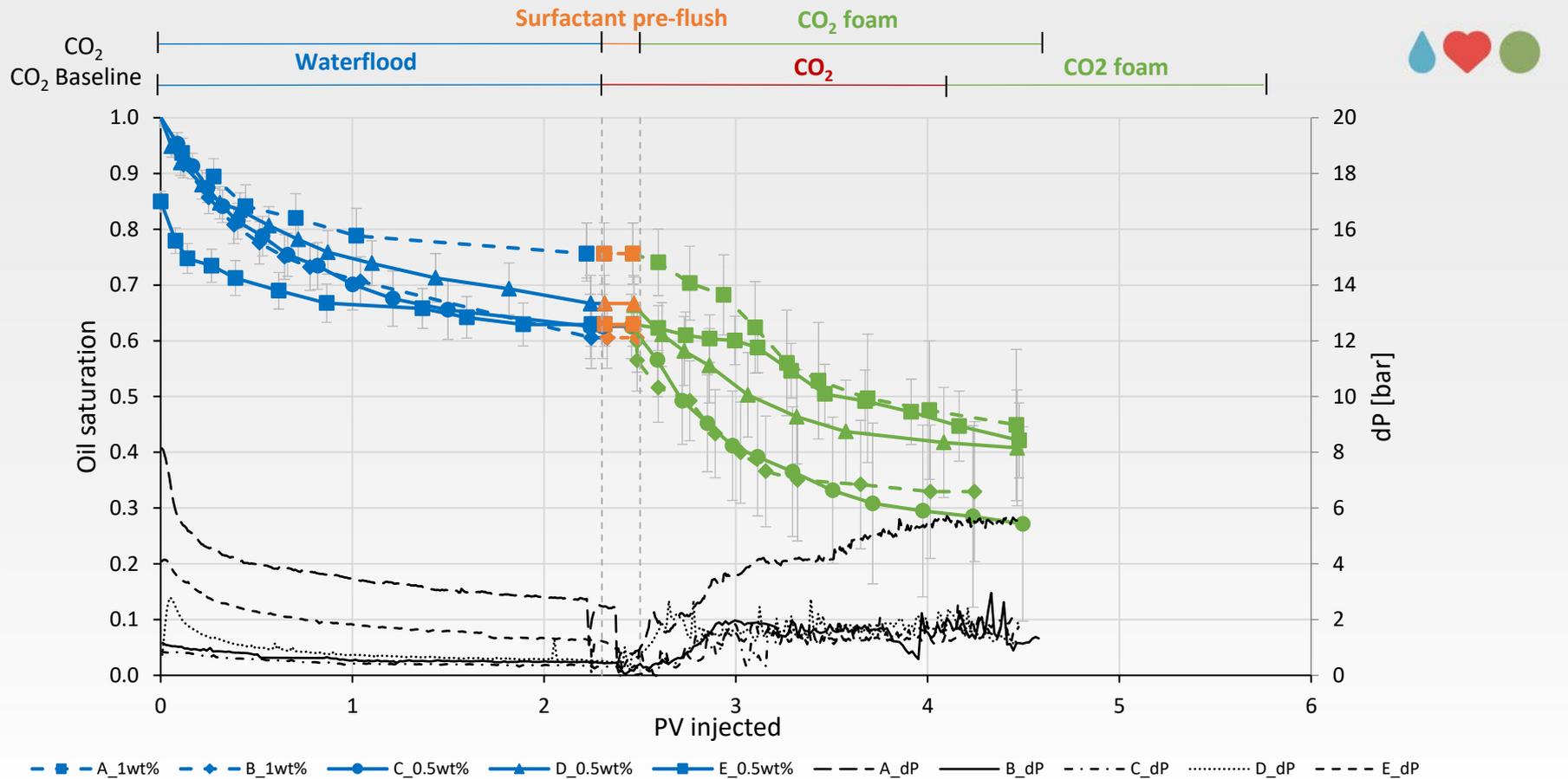
Experimental conditions and procedure:

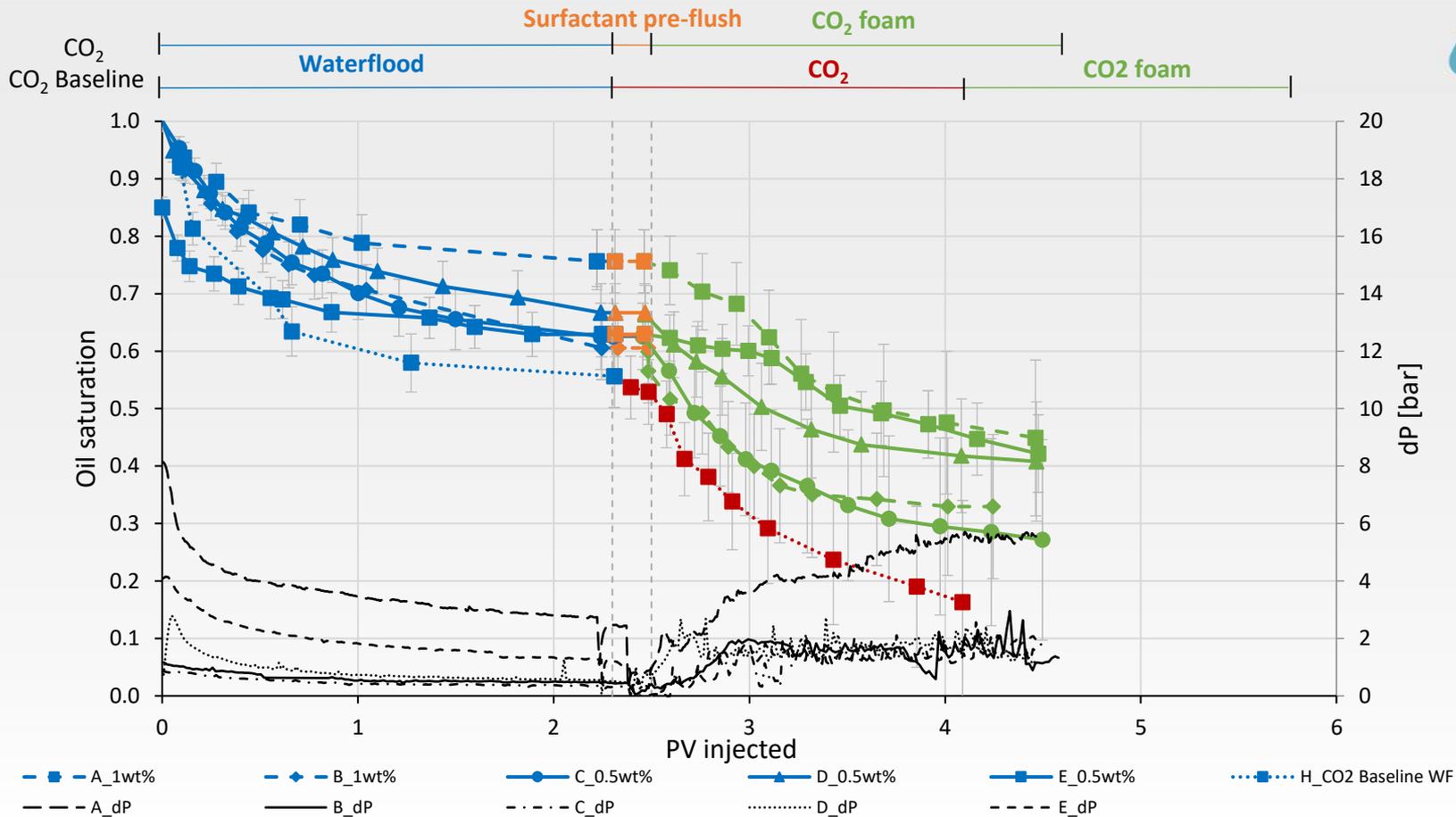
2500 psi at 40°C

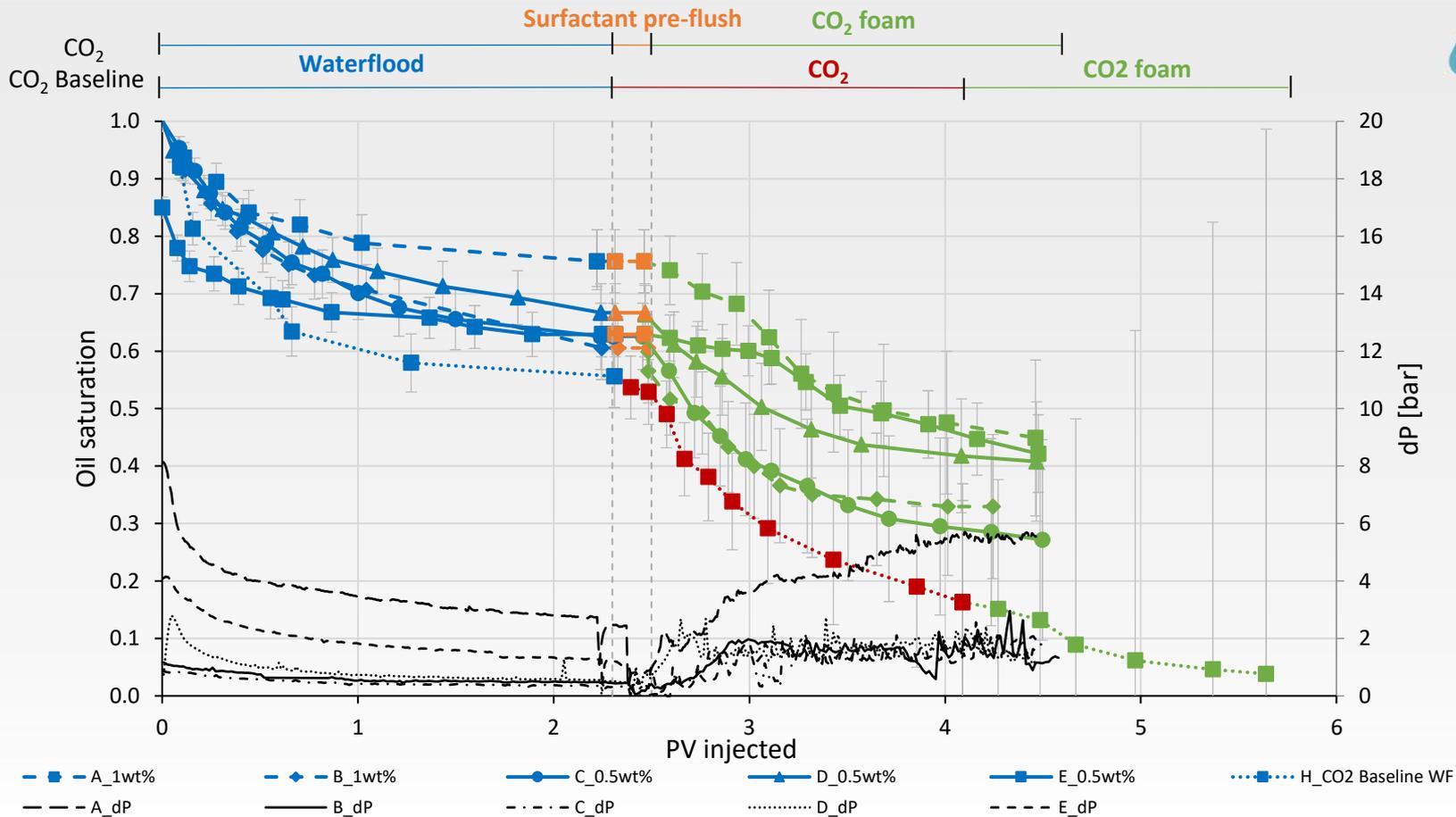
Reservoir-core was restored to reservoir conditions and 100% oil saturated.

Initial **waterflood**, **surfactant pre-flush**, **CO₂ flood**, and a final **CO₂ foam** flood.

All rates were 1 ft/D, at a gas fraction of 0.70.







Associated CO₂ Storage – Reservoir Cores

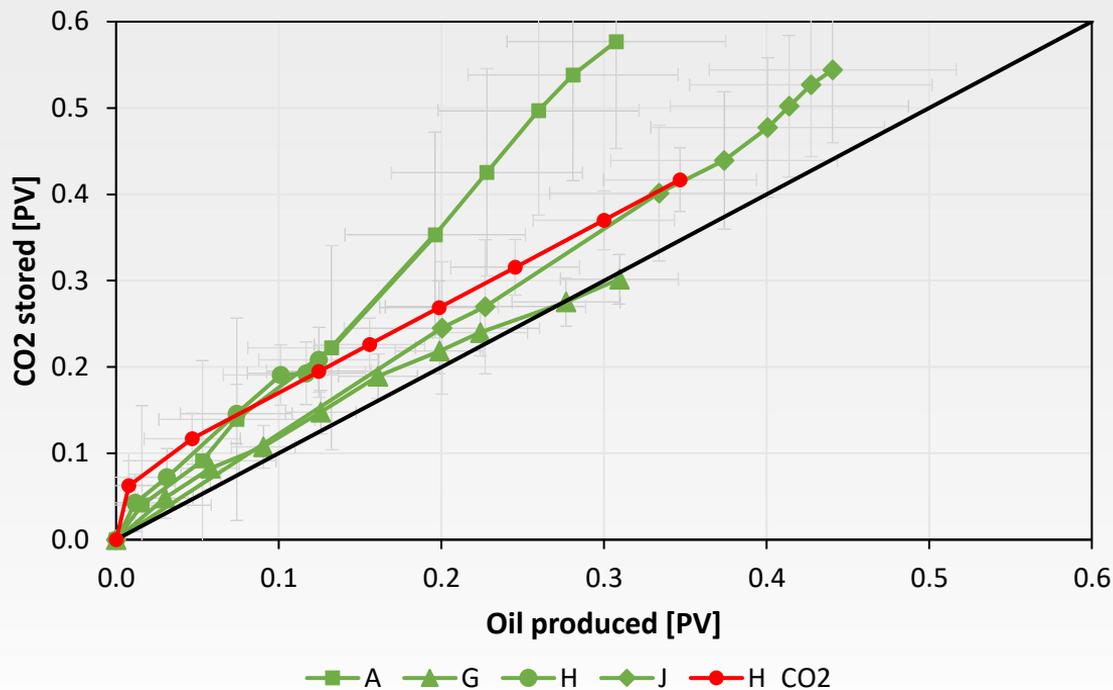


CO₂ storage during CO₂ foam displacement (after WF)

40°C, 2500 psi

Oil-wet

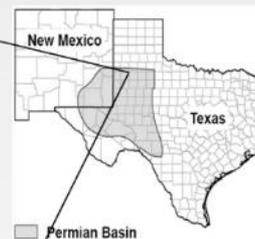
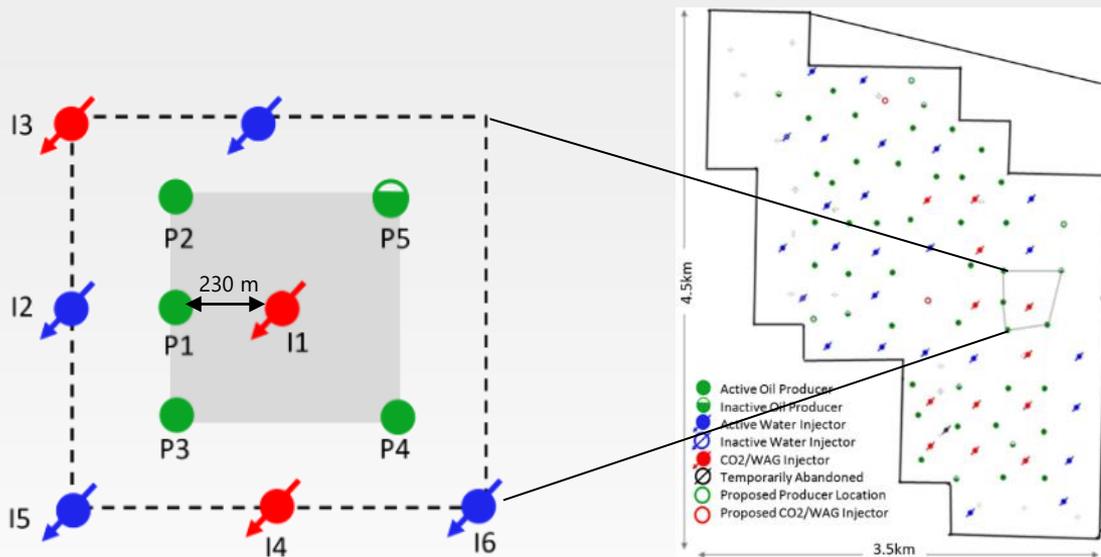
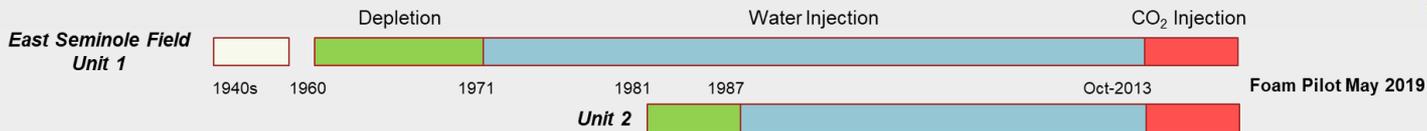
Foam displaces water in favor of CO₂ storage





The Pilot

Pilot Pattern



San Andres Dolomite

Reservoir Characteristic	Value
Depth	5200 ft
Permeability	1 to 250 md (avg: 13 md)
Porosity	3% to 28% (average: 12%)
Pay thickness	110 ft
Reservoir pressure (initial)	2500 psig
Reservoir pressure (current)	3400 psig
Fracture pressure	3900 psig
Reservoir temperature	104°F
Oil gravity	31 °API
Formation brine salinity	70,000 ppm

Rapid CO₂ Breakthrough
High producing GOR

Pilot Design

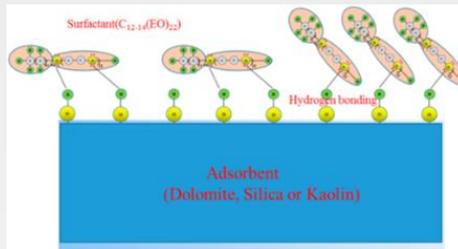


Foam Formulation

- Minimal adsorption
- Adequate foam strength
- Chemical stability

Nonionic Surfonic L24-22, a linear ethoxylated alcohol ($C_{12-14}E_{22}$)

Foam quality: 60% to 70%
Surfactant concentration: 0.5 wt%



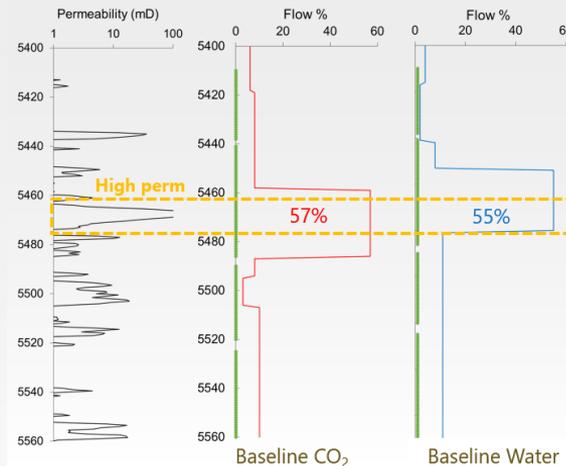
Injection Strategy

Surfactant alternating gas (SAG):
10 days surfactant, 20 days CO_2
Half the historical injection rate

San Andres

Reservoir Characteristic	Value
Depth	5200 ft
Permeability	1 to 250 md (avg: 13 md)
Porosity	3% to 28% (average: 12%)
Pay thickness	110 ft
Reservoir pressure (initial)	2500 psig
Reservoir pressure (current)	3400 psig
Fracture pressure	3900 psig
Reservoir temperature	104°F
Oil gravity	31 °API
Formation brine salinity	70,000 ppm

Baseline (pre-pilot) injection profiles



Pilot start: May 2019

Pilot end: August 2020

May 2021

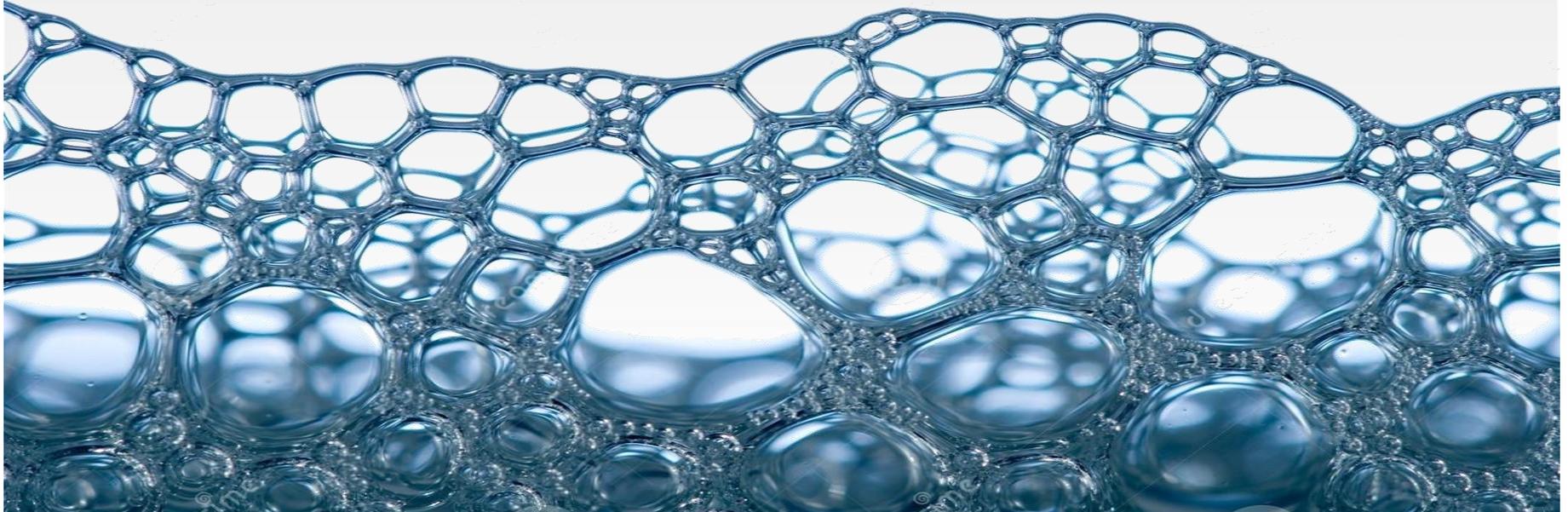


Pilot Objectives



In-depth CO₂ mobility control

Improve CO₂ sweep efficiency, oil recovery and CO₂ utilization





Data Collection and Monitoring

Data Collection and Pilot Monitoring



- Obtain baseline and monitor pilot performance to evaluate reservoir response to foam injection.
- Characterize **interwell connectivity** and CO₂ and water injectivity.

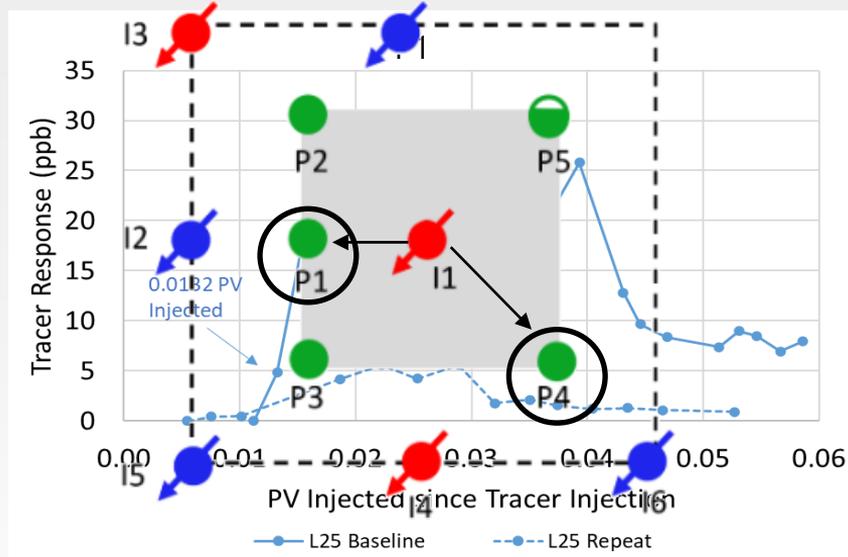
	SAG Cycle													
	Pre	1	2	3	4	5	6	7	8	9	10	11	Post	
Slug	Water	CO2	Surfactant	Water										
IWTT		x											x	
Injection Profiles	x	x		x	x				x	x		x	x	x
Produced water collection			x	x	x	x	x	x	x	x	x	x	x	x
DHPG reading		x		x				x					x	x

Water	CO2	Surfactant
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CO₂ Interwell Tracer Test (IWTT)

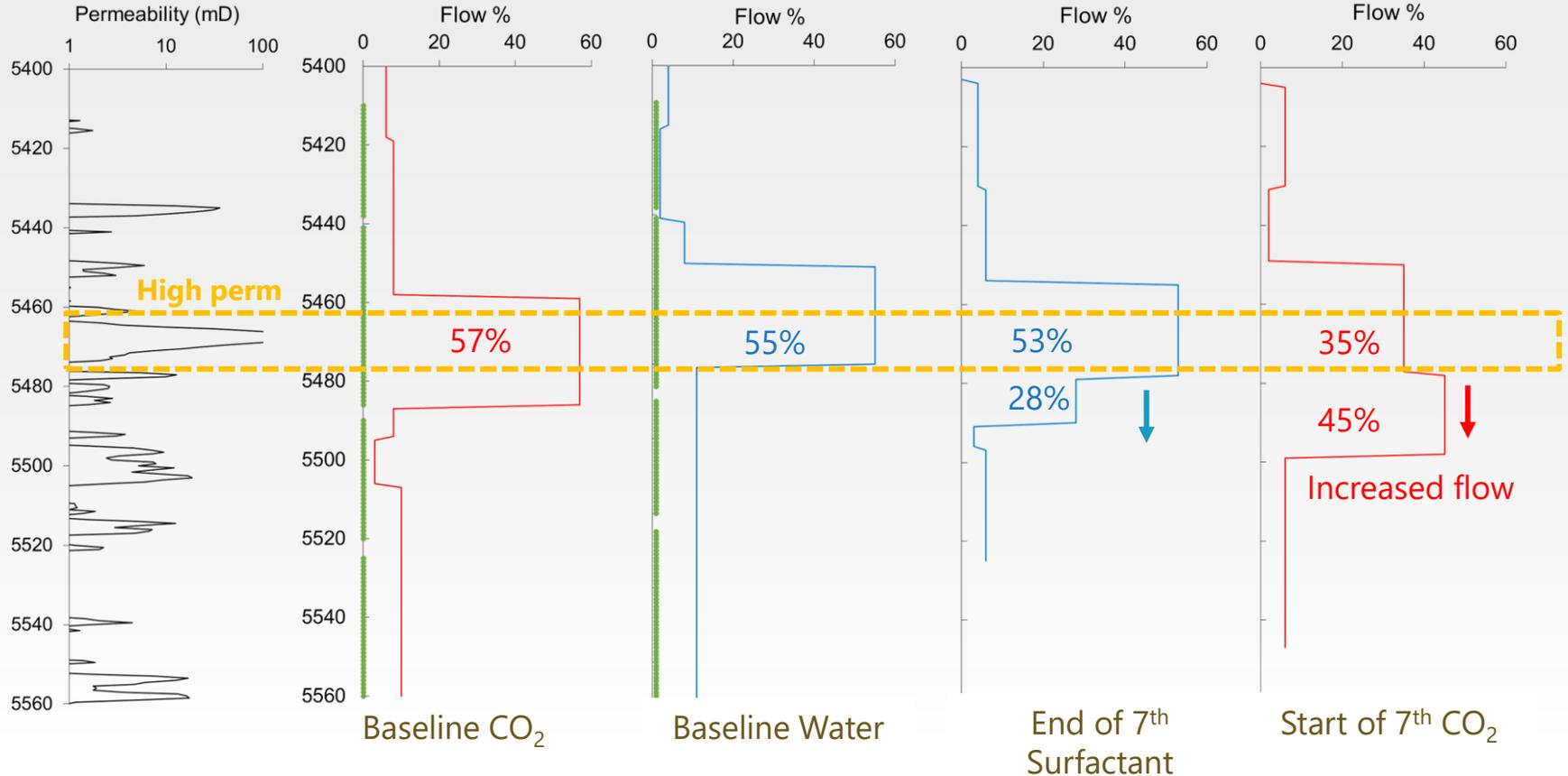


- Determine baseline CO₂ breakthrough time (BT) and migration rate
- Compare it to BT time after foam injection

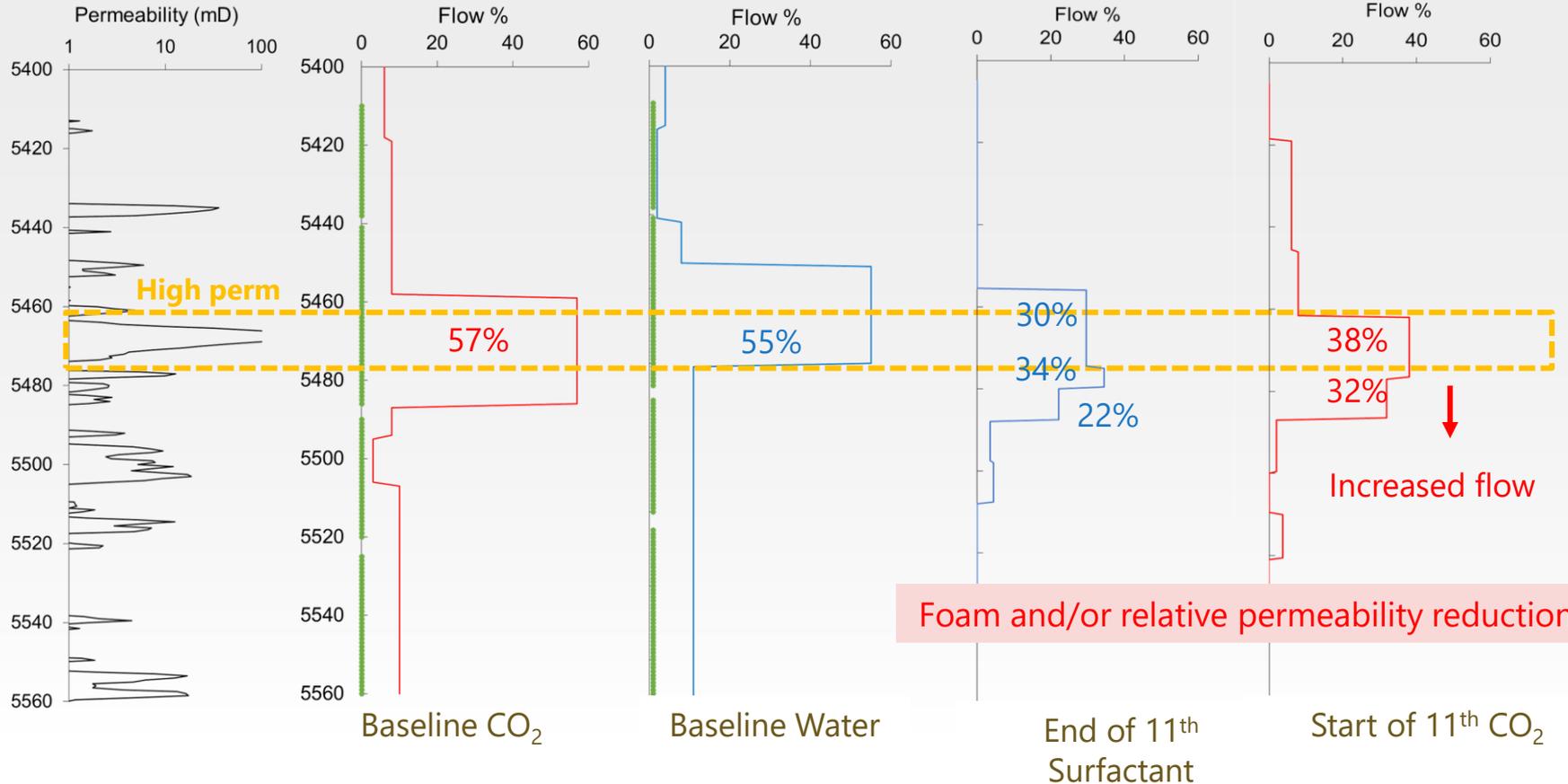


- CO₂ breakthrough from I1 to P1 delayed by 43% during the foam pilot
- Baseline tracers broke through at a higher concentration
 - Tracers during foam injection mostly went through matrix due to reduced CO₂ channeling in a high-permeability zone

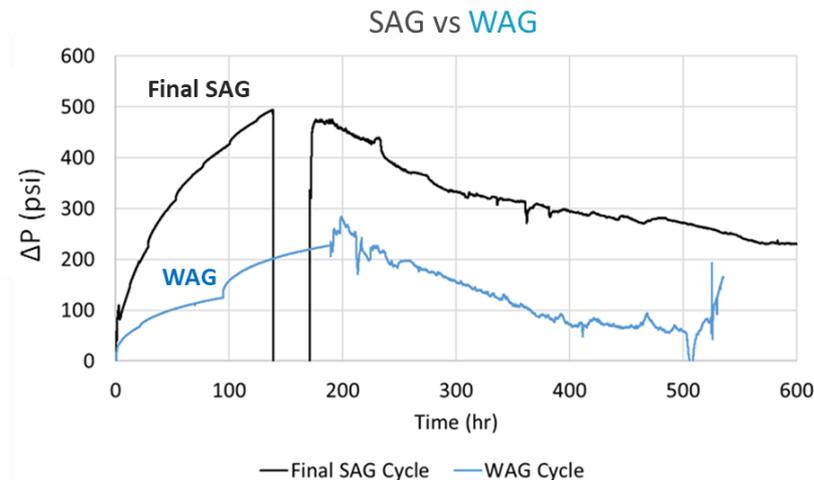
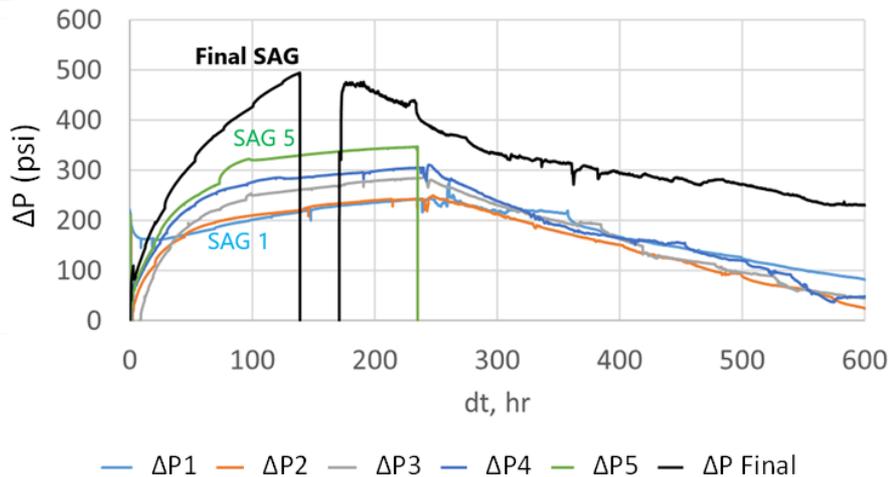
Injection Profiles – Foam Injector



Injection Profiles – Foam Injector



Transient Analysis



Reduced mobility of each cycle, indicating a foam bank developing further into the reservoir.

Reduced mobility during the SAG cycles compared to the WAG

Pilot start: May 2019

Pilot end: August 2020

May 2021



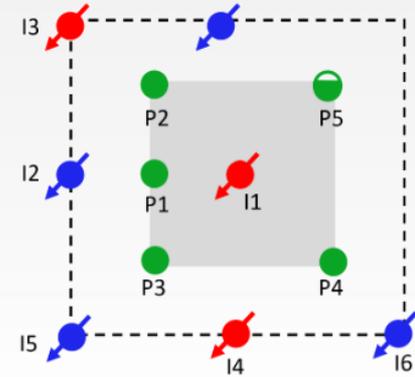
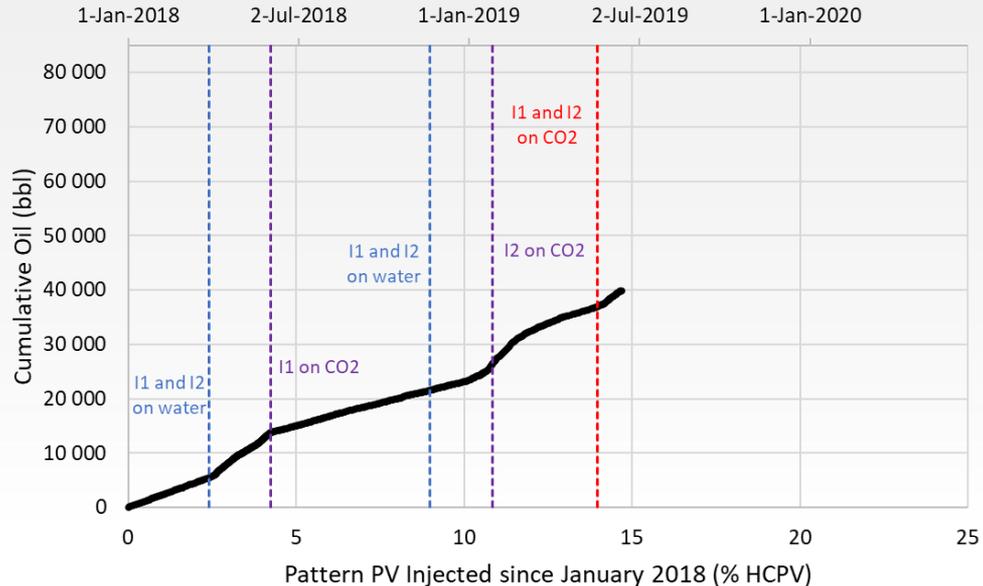


Production Analysis

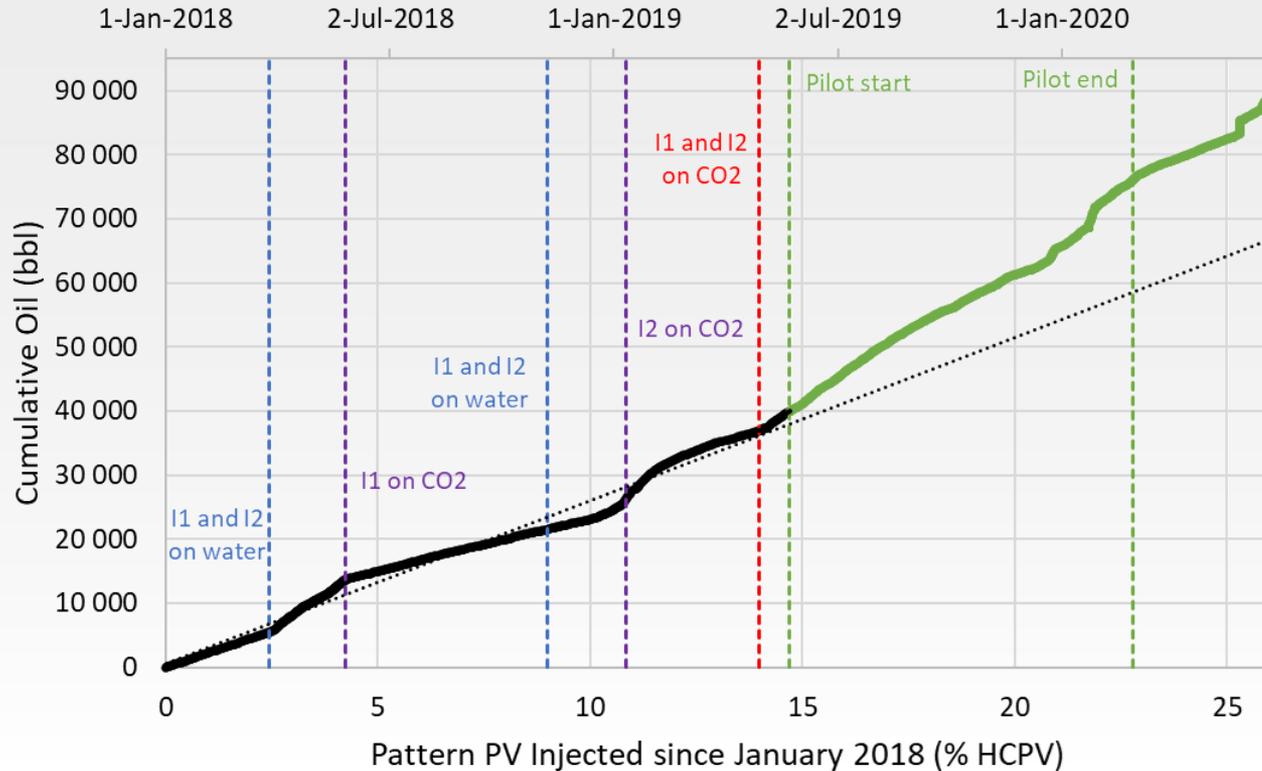
Production Analysis



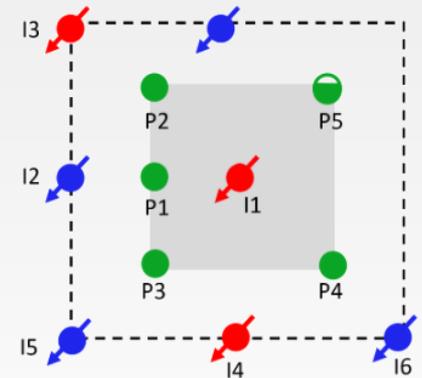
- Cumulative oil recovered as a function of pore volume injected.
- Projection of the baseline performance.
 - 1.5 years prior to the start of the pilot (January 2018 to May 2019) with consistent data and minimal operational disruptions in the pattern.



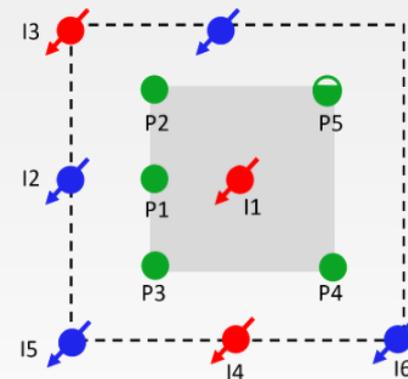
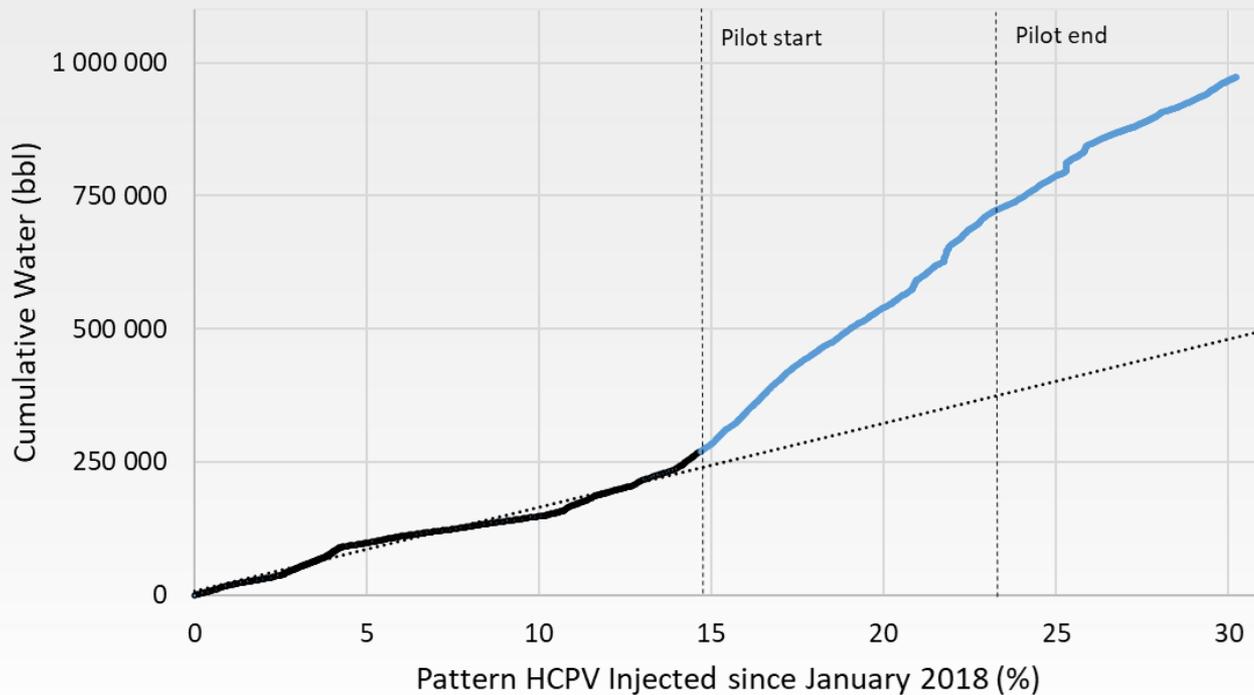
Production Analysis – Pilot Pattern



+25,000 bbls



Production Analysis – Pilot Pattern



Conclusions



Reduced CO₂ mobility

Increased sweep efficiency

Improved oil recovery

Increased CO₂ storage volumes

Ongoing monitoring and analysis

Acknowledgements



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