

# **CO<sub>2</sub> Foam EOR, Mobility Control**

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**ADNOC**

**4<sup>th</sup> Biennial CO<sub>2</sub> for EOR as CCUS Conference 2019**

**Rice University**

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# **Challenges of CO<sub>2</sub> Mobility Control in Middle East**

- **High temperatures: >100 °C**
- **High Salinity: > 20% ppm TDS**
- **High MMP: >3,000 psi**
- **Carbonate formations**

# **Outline of Presentation**

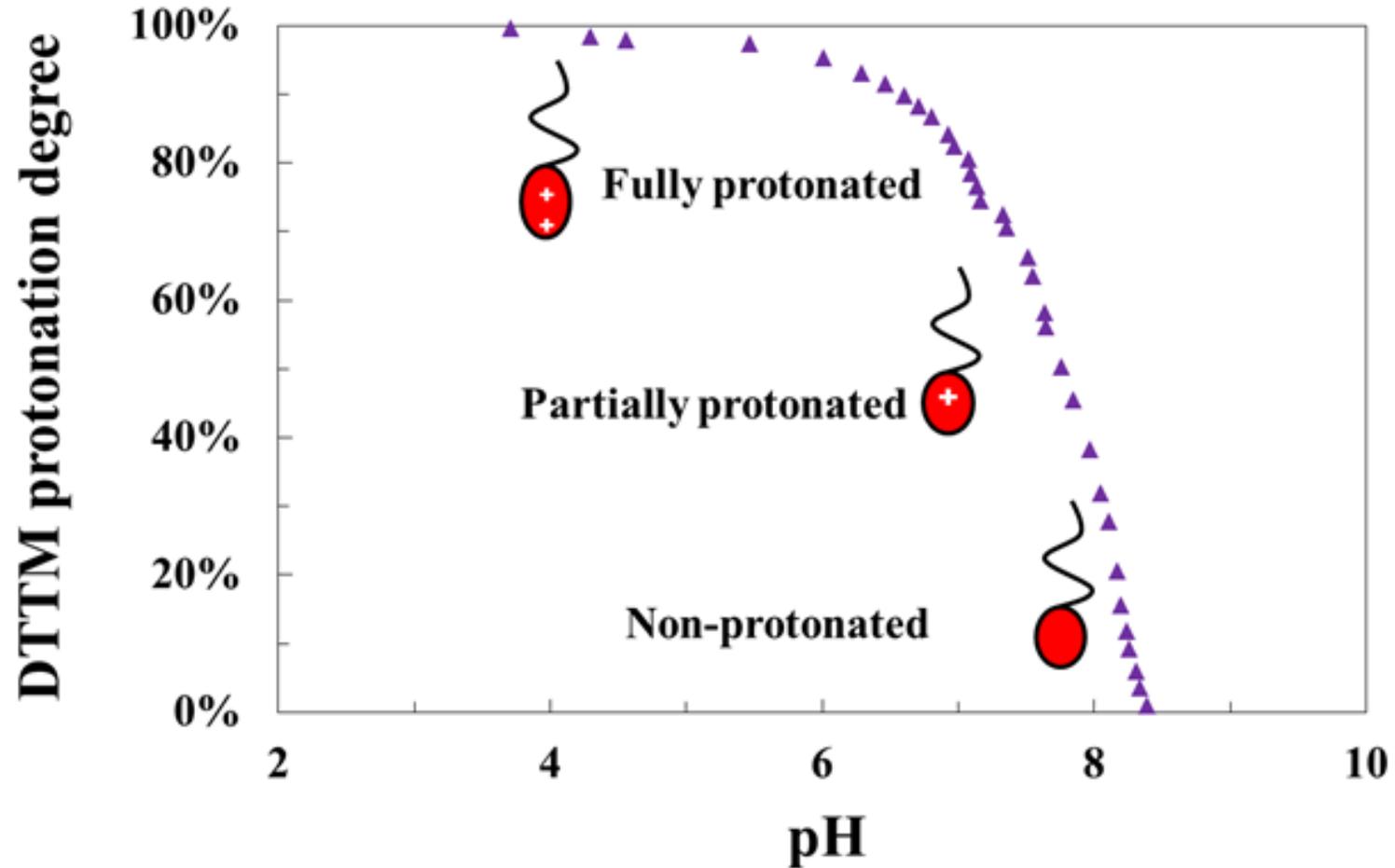
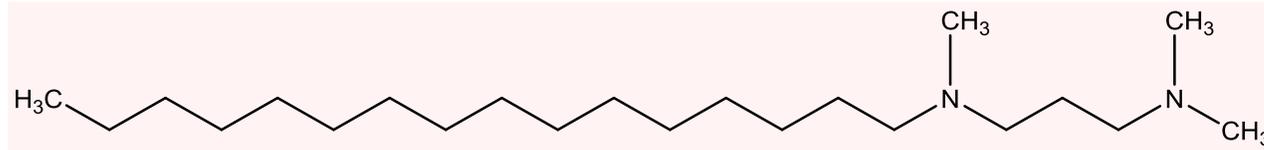
- **Surfactant stability and adsorption**
- **In situ foam generation by co-injection and SAG**
- **Estimation of foam parameters for simulation**
  - **Foam dry-out**
  - **Shear thinning**
  - **Surfactant concentration**
  - **Effect of crude oil**
- **Simulation of oil displacement in heterogeneous reservoir**
- **Conclusions**

# **Surfactant Stability & Adsorption**

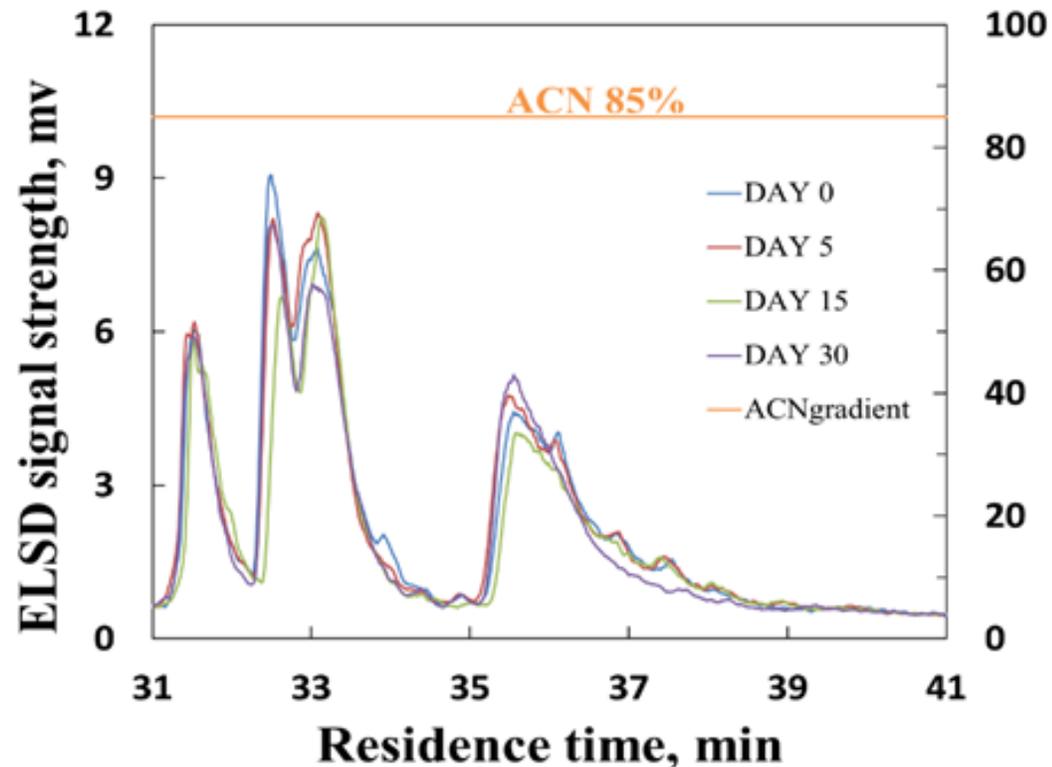
- **Anionic surfactant – Excessive adsorption on carbonates**
- **Nonionic surfactant – Above cloud point temperature**
- **Switchable cationic, Ethomeen C/12\* – Minimum pressure gradient for foam generation**
- **Duomeen TTM\* – Evaluated here**

**\* Trademark of AkzoNobel**

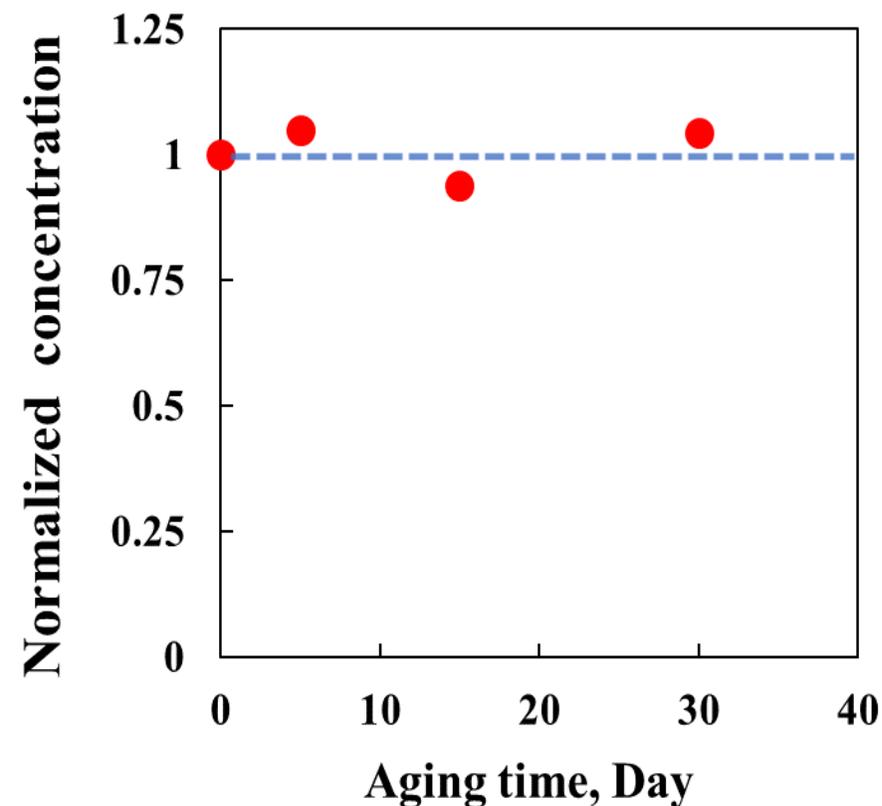
# DTTM is fully protonated at the pH of CO<sub>2</sub> saturated brine



# TTM is stable at 120 °C in presence of oxygen scavenger

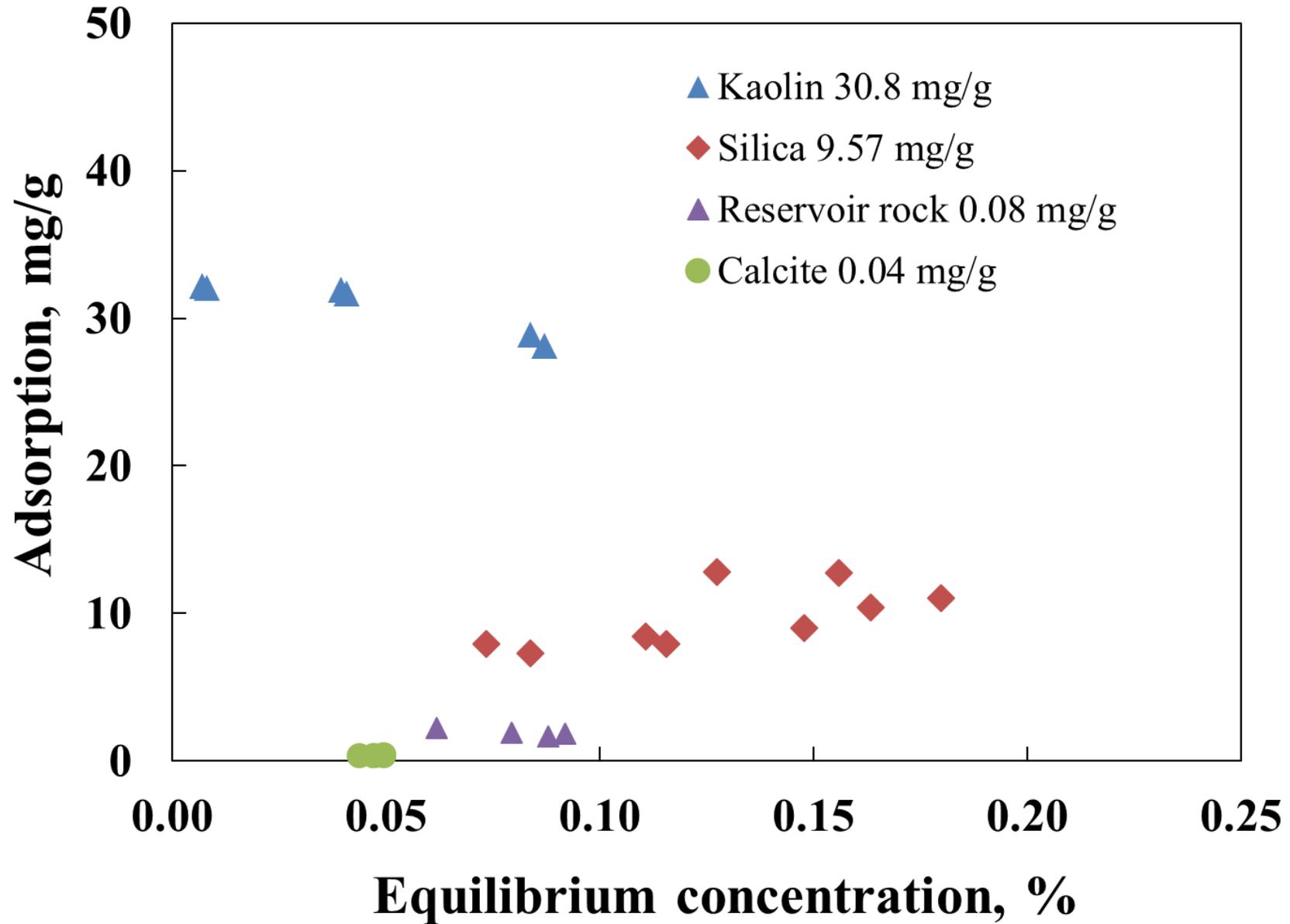


1 DTTM characteristic peaks and signal strength as a function of aging time at 120°C, Formation Brine, pH4, and reducing conditions.

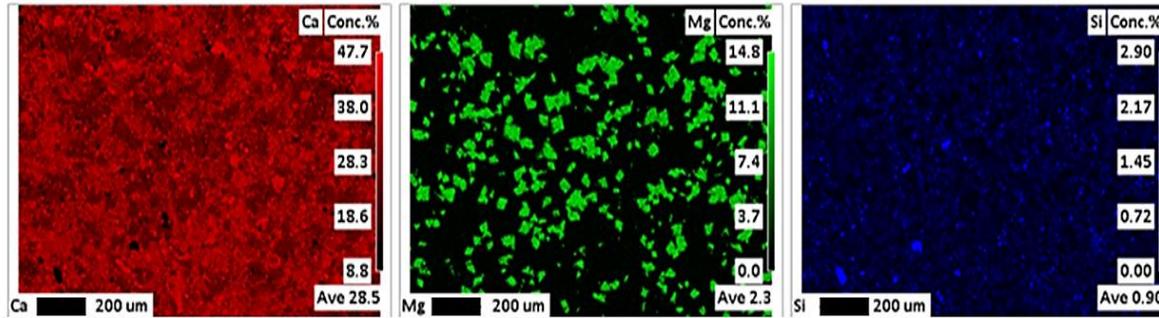


DTTM signal integral area as a function of aging time, the areal variation is within the detection error.

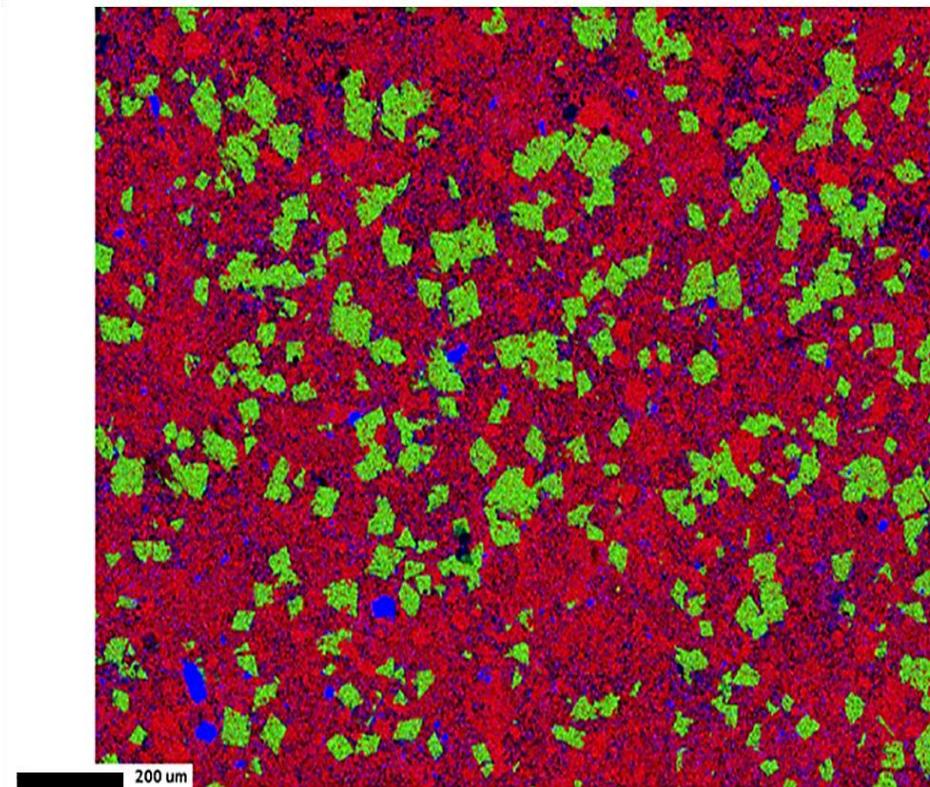
# Measured Adsorption of TTM



# Elemental Composition of Reservoir Rock



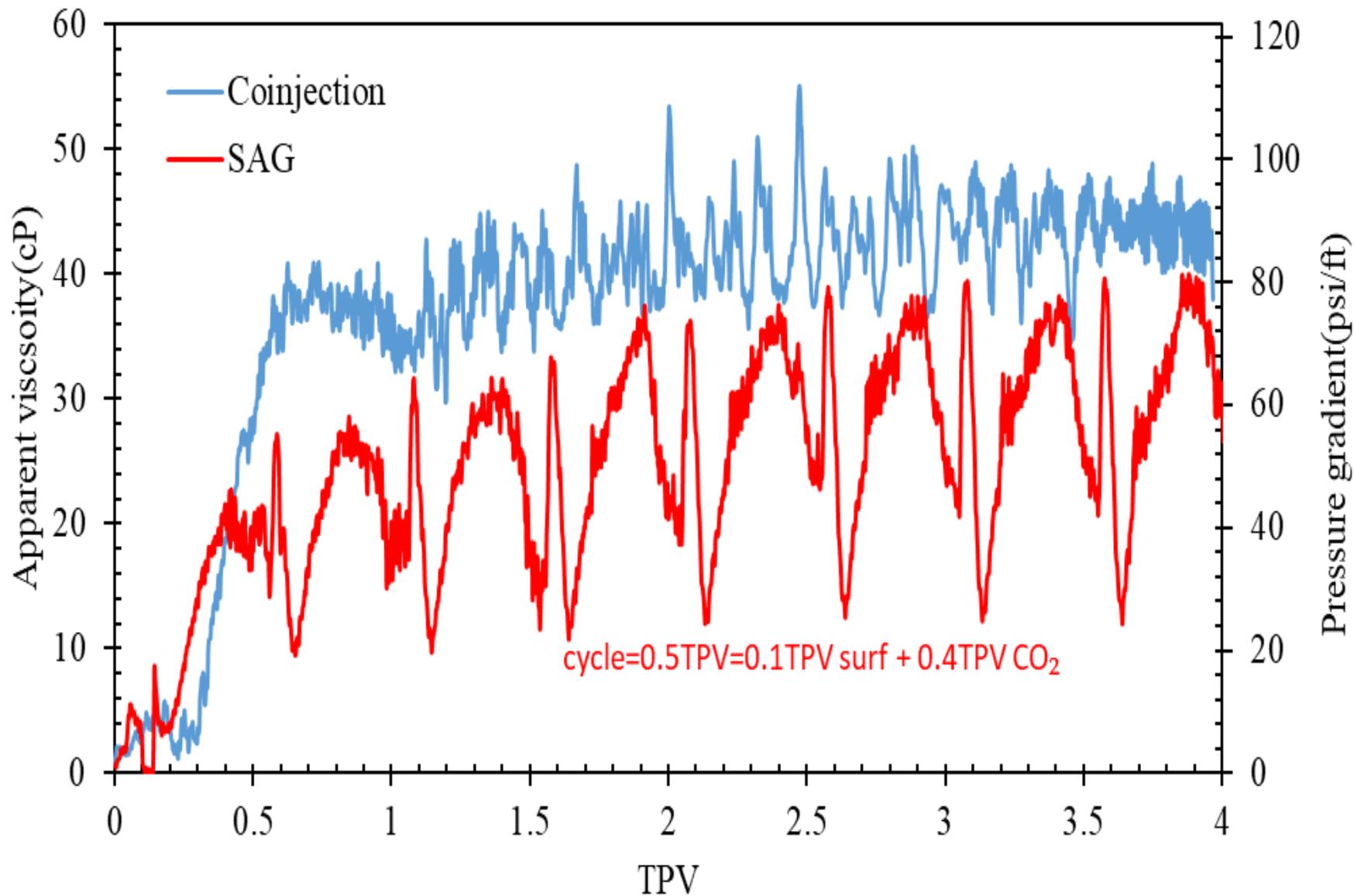
**Ca 25%, Mg 2.8%, Si 0.7%**



**Red – Ca**  
**Green – Mg**  
**Blue - Si**

# In situ foam generation without oil

3,400 psi,  
120 °C.  
Foam quality=80%,  
4ft/day  
1% TTM in 22% TDS Brine,  
L\*D=3\*1.5 inches,  
k=321 mD



# Dry-out function parameters(1%TTM)

$$FM = \frac{1}{1 + fmmob \times \left\{ 0.5 + \frac{\arctan[epdry(S_w - fmdry)]}{\pi} \right\}}$$

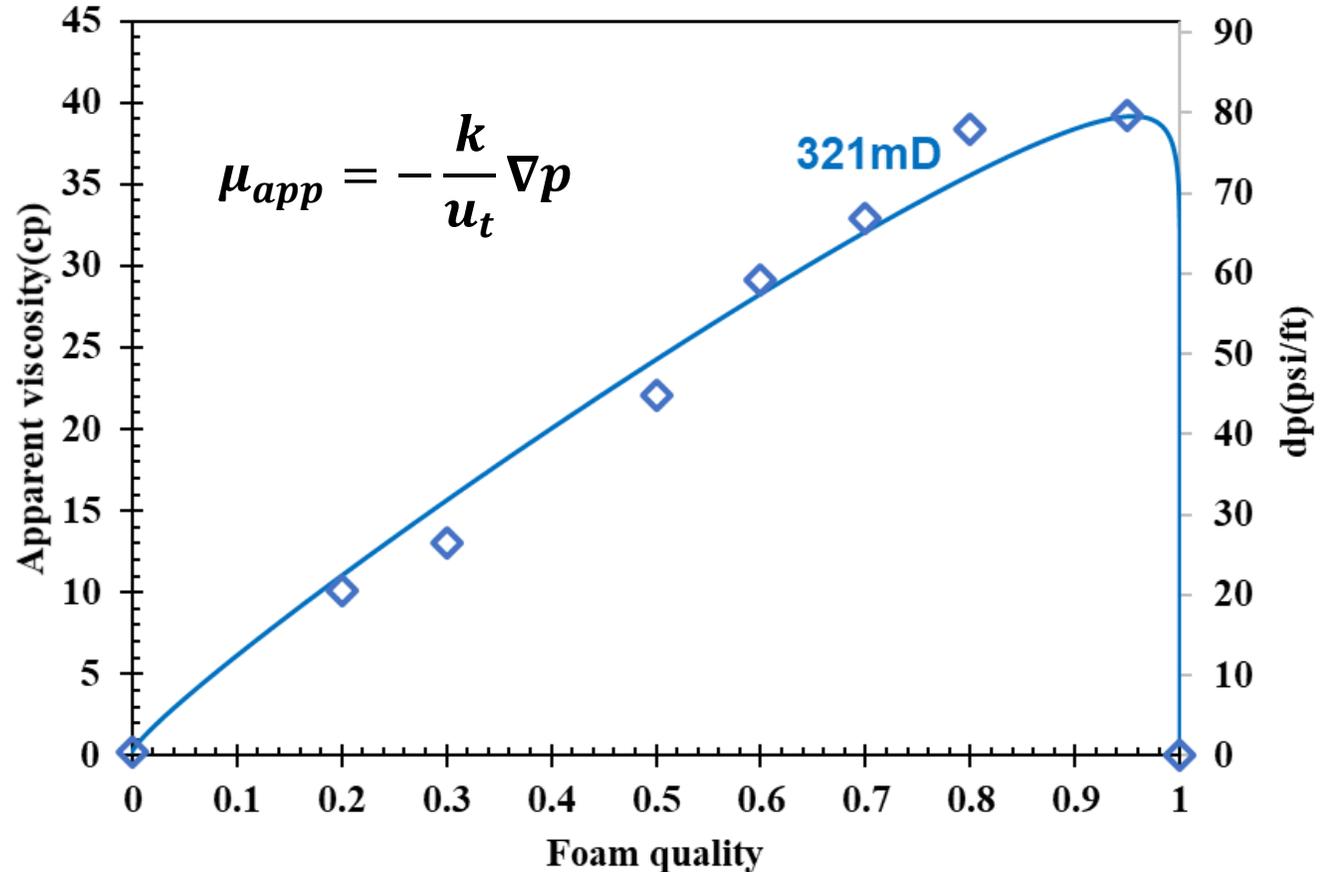
*k(mD) fmmob epdry fmdry*

321	188	70	0.238
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## Experimental conditions

- 1% TTM, pH=7
- 120 °C
- 3,400 psi
- 4 ft/day
- Indiana Limestone(321mD)

Experiment and STARS model(1% TTM)



$$f_g = \frac{u_g}{u_w + u_g} = \frac{u_g}{u_t}$$

# Shear thinning parameters

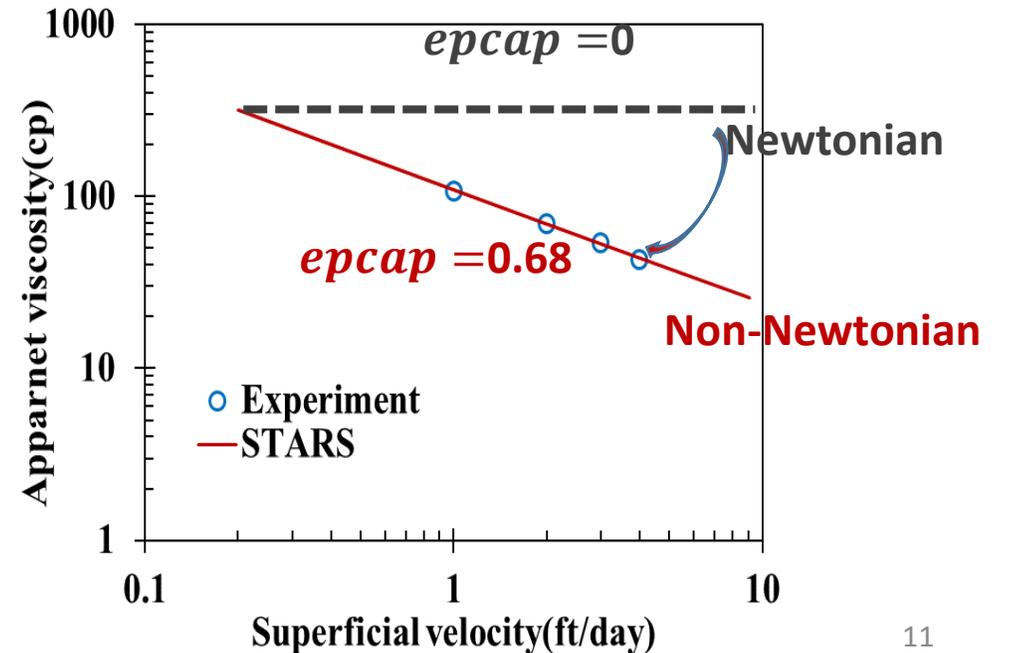
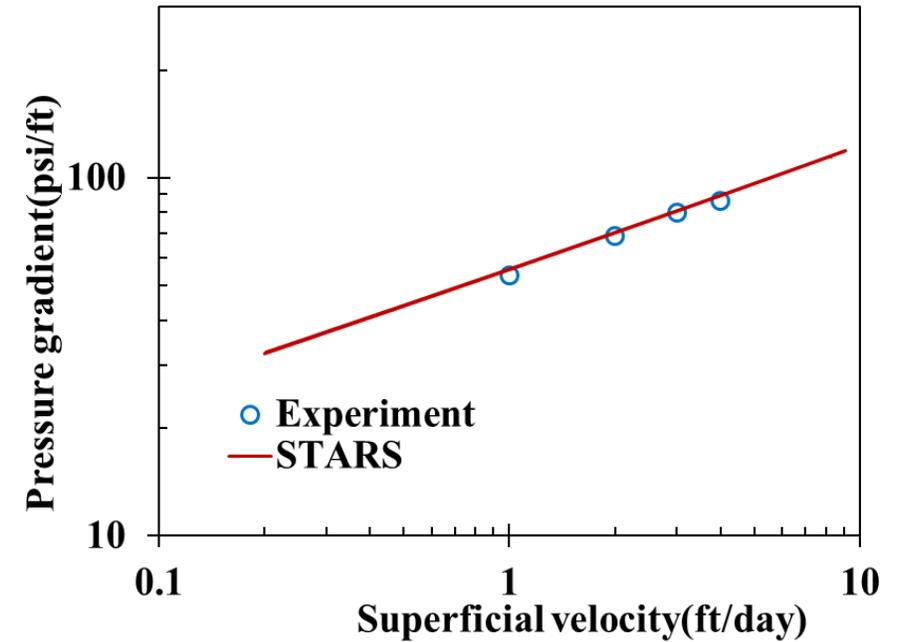
$$FM = \frac{1}{1 + fmmob \times Fwater \times \left(\frac{fmcap}{NCa}\right)^{epcap}}$$

*fmcap*      *epcap*

1.17e-06      0.68

## Experimental conditions

- 1% TTM, pH=7
- 120 °C
- 3,400 psi
- 1~4 ft/day
- fg=0.8
- Indiana Limestone(321mD)



# Surfactant concentration parameters

**FM**

$$= \frac{1}{1 + f_{mob} \times F_{water} \times \left( \frac{C_{sw}}{f_{msurf}} \right)^{epsurf}}$$

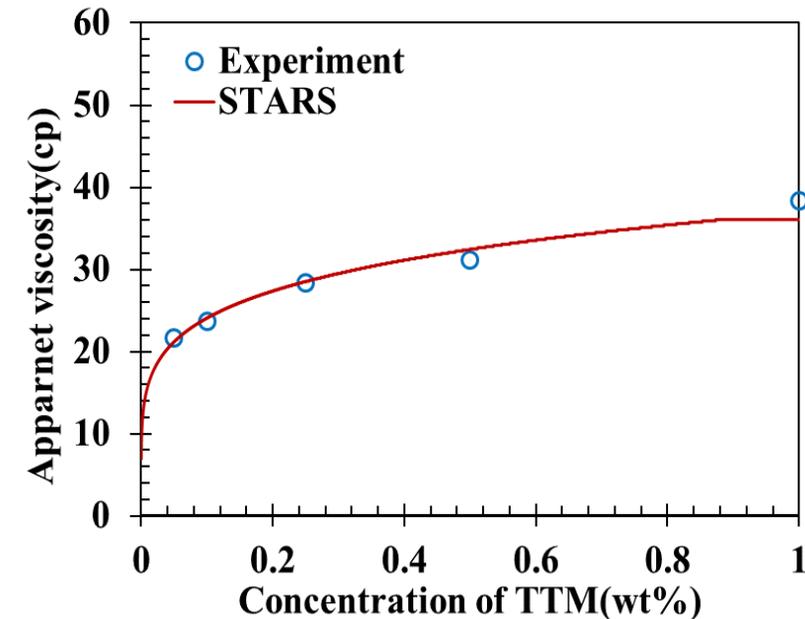
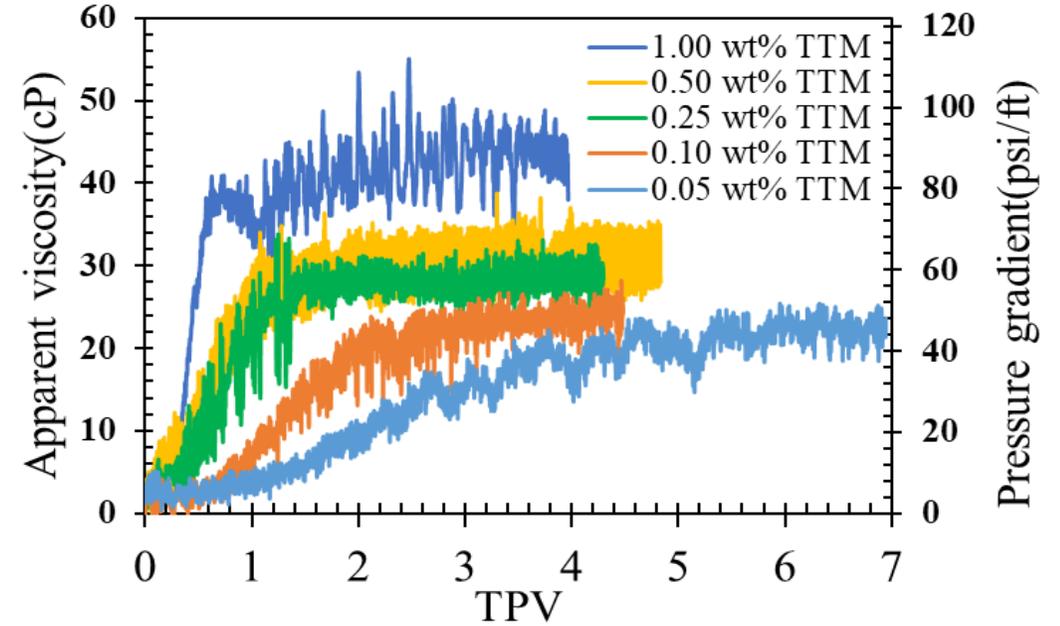
*f<sub>msurf</sub>*      *epsurf*

0.89 wt%      0.195

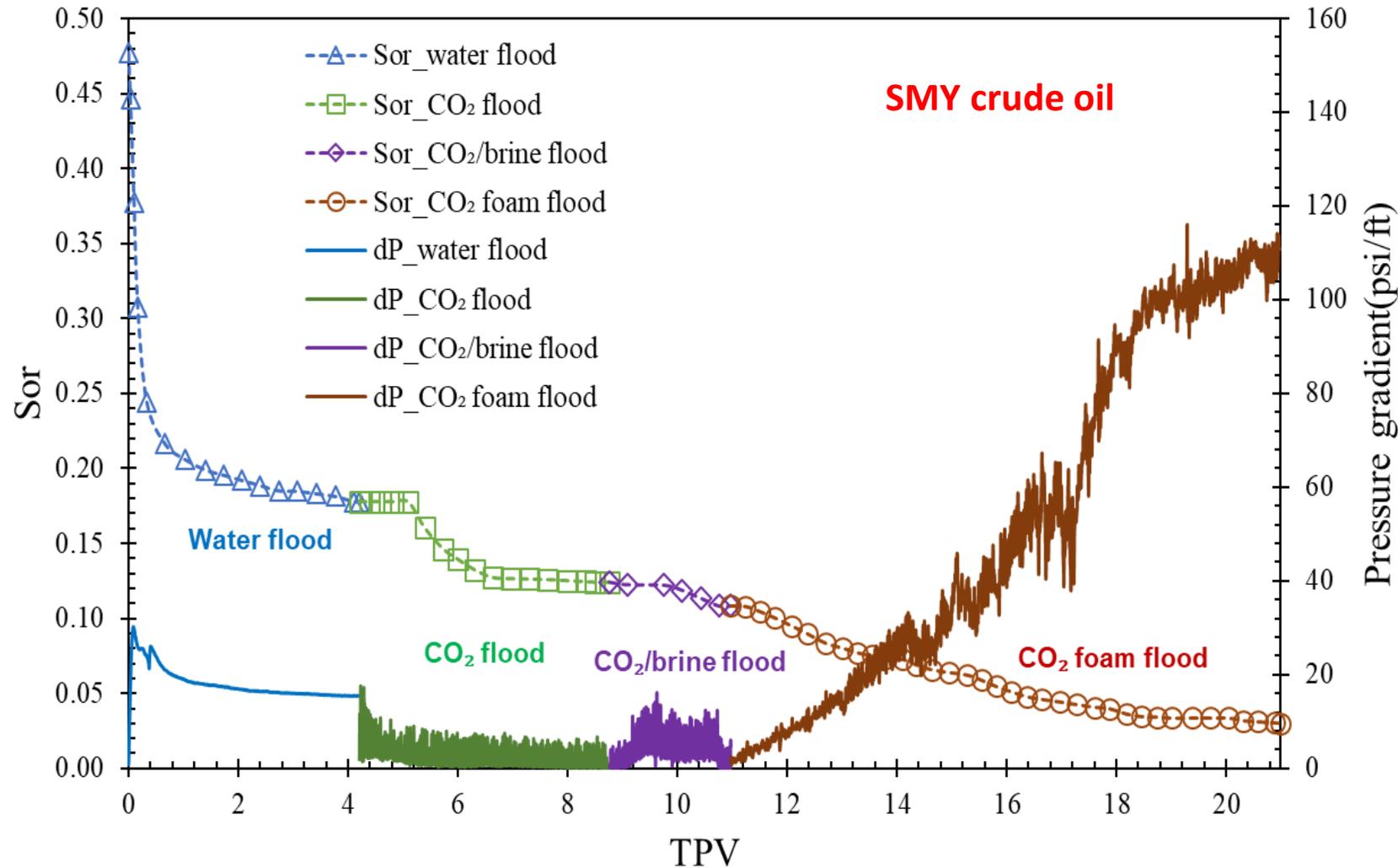
### Experimental conditions

- 0.1~1% TTM, pH=7
- 120 °C
- 3400 psi
- 4 ft/day
- fg=0.8
- Indiana Limestone(321mD)

Conc. effect on TTM(pH=7) CO<sub>2</sub> foam



# CO<sub>2</sub> foam EOR by TTM

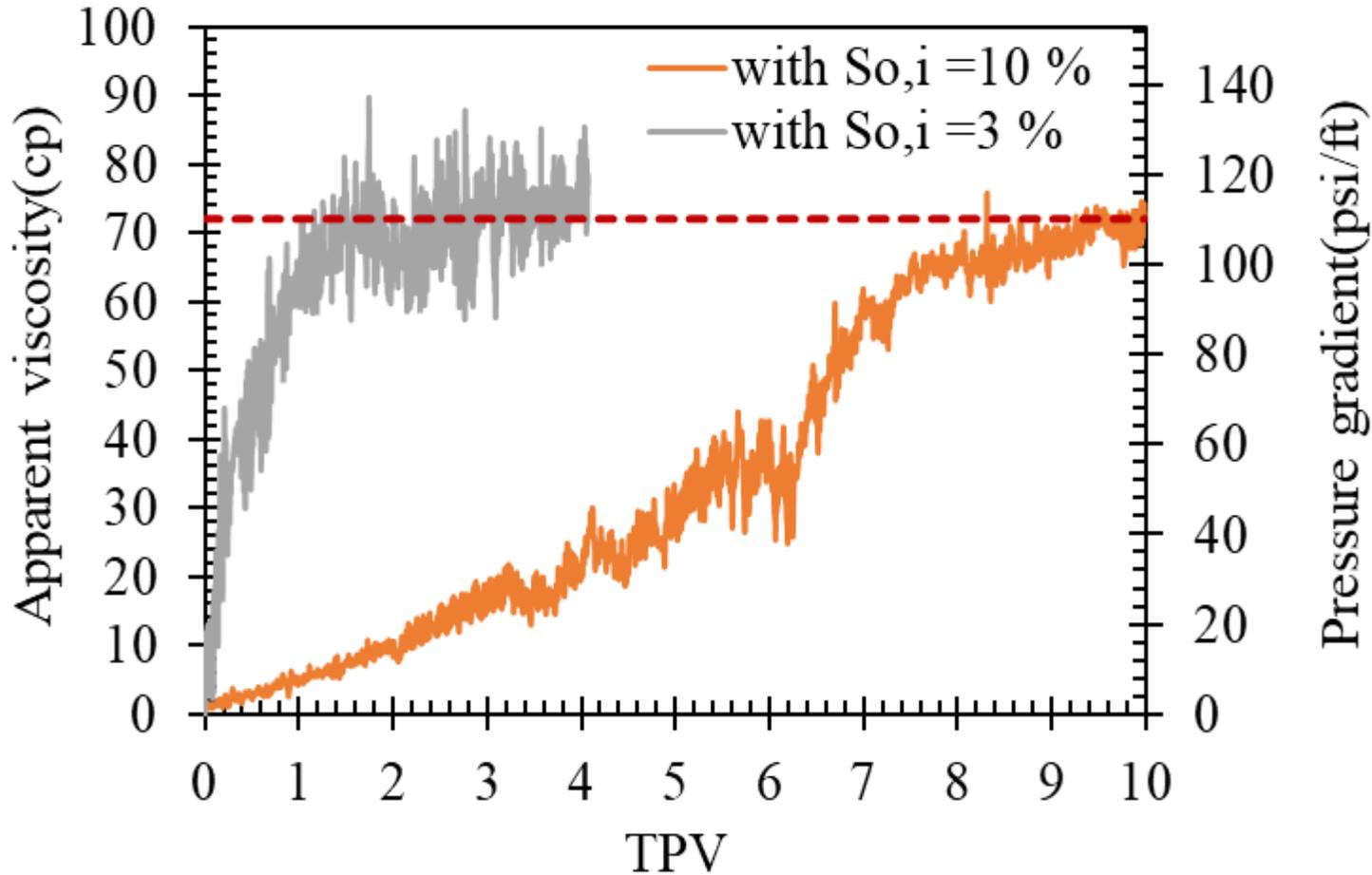


## Experimental conditions

- k=413 mD (L\*D=6\*1.5 inch)
- 4ft/day
- fg=0.8
- 1 wt% TTM
- 120°C
- 3400 psi
- **SMY crude oil**

Oil saturation and pressure gradient for water, CO<sub>2</sub>, CO<sub>2</sub>-brine, and CO<sub>2</sub> foam flooding in an Indiana limestone core

# Effect of crude oil saturation on CO<sub>2</sub> foam generation

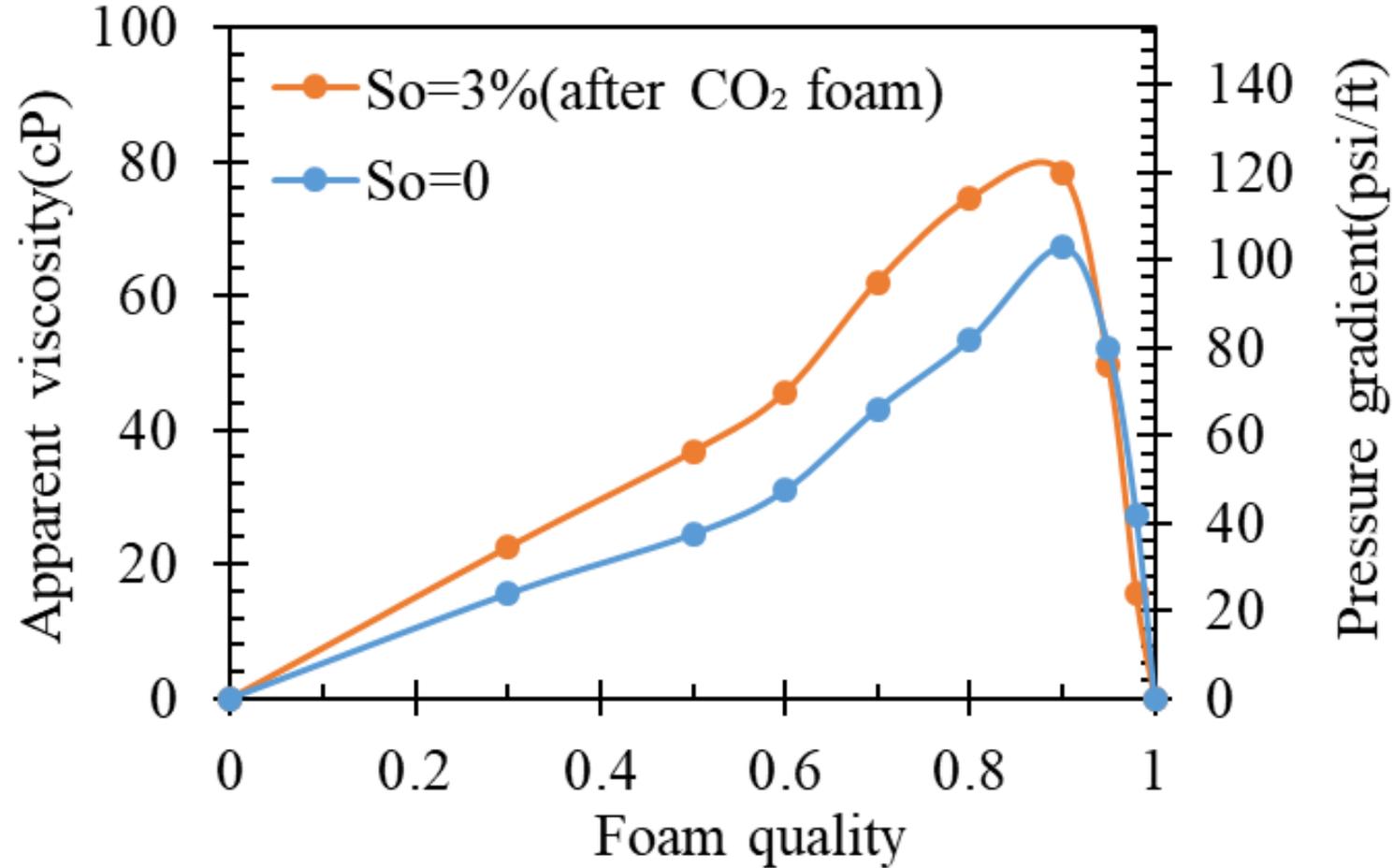


## Experimental conditions

- $k=413$  mD ( $L \cdot D=6 \cdot 1.5$  inch)
- 4ft/day
- $fg=0.8$
- 1 wt% TTM
- 120°C
- 3400 psi
- **SMY crude oil**

CO<sub>2</sub> foam apparent viscosity at an initial crude oil saturation of 3% (grey) and 10% (orange) in an Indiana limestone core

# Effect of residual oil saturation on CO<sub>2</sub> foam quality scan

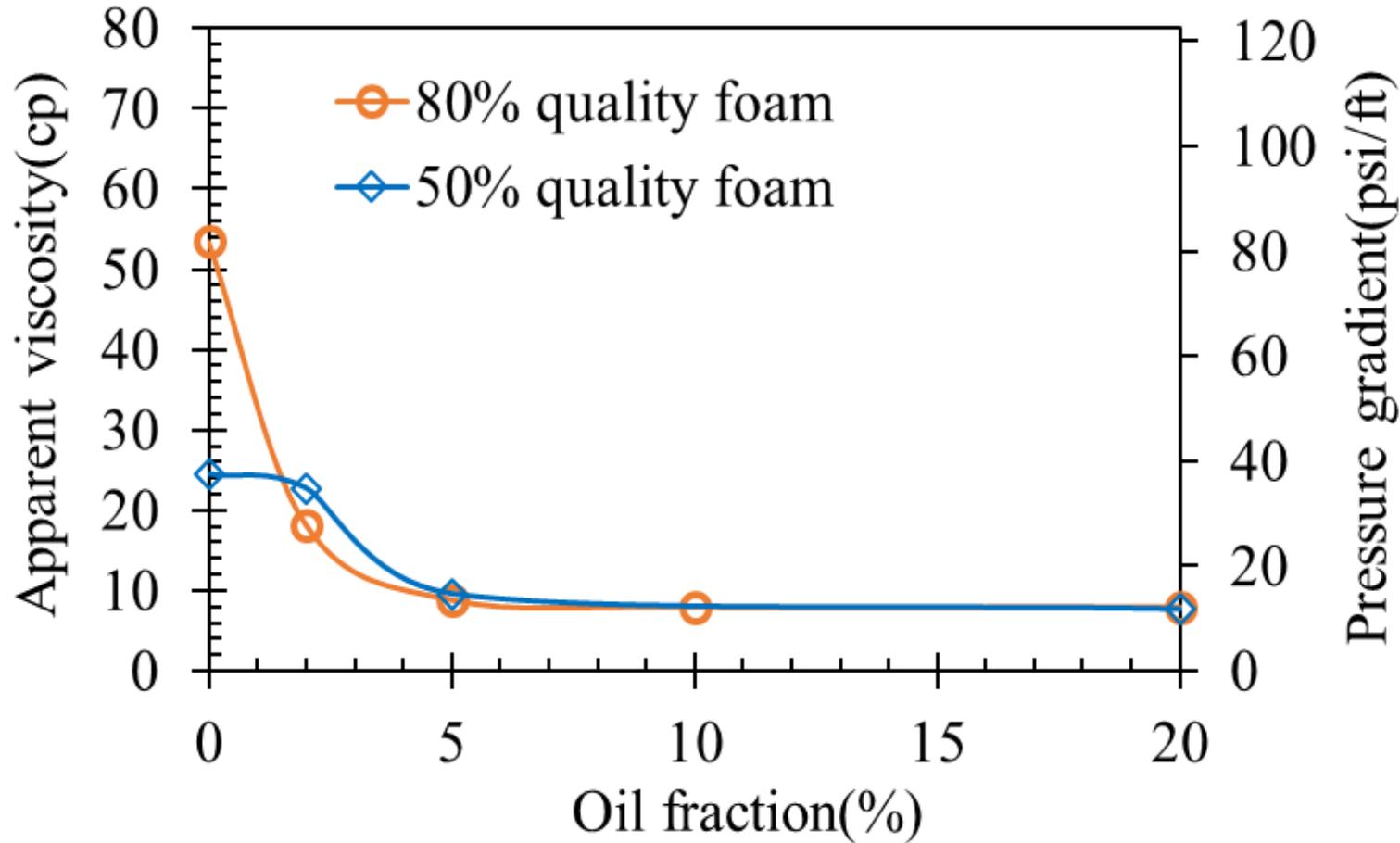


## Experimental conditions

- $k=413$  mD ( $L \cdot D=6 \cdot 1.5$  inch)
- 4ft/day
- $fg=0.8$
- 1 wt% TTM
- 120°C
- 3400 psi
- **SMY crude oil**

A CO<sub>2</sub> foam quality with 1 wt% TTM scan without oil and with 3% crude oil present, in an Indiana limestone core

# Effect of oil fractional flow on foam strength



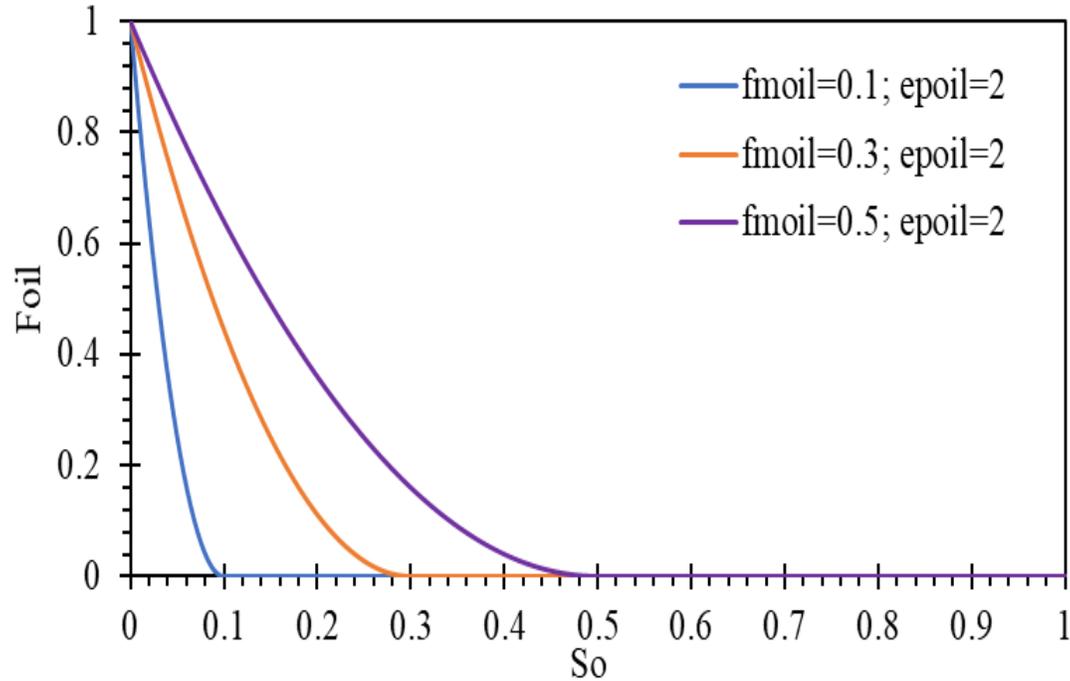
## Experimental conditions

- $k=413$  mD ( $L \cdot D=6 \cdot 1.5$  inch)
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- 120°C
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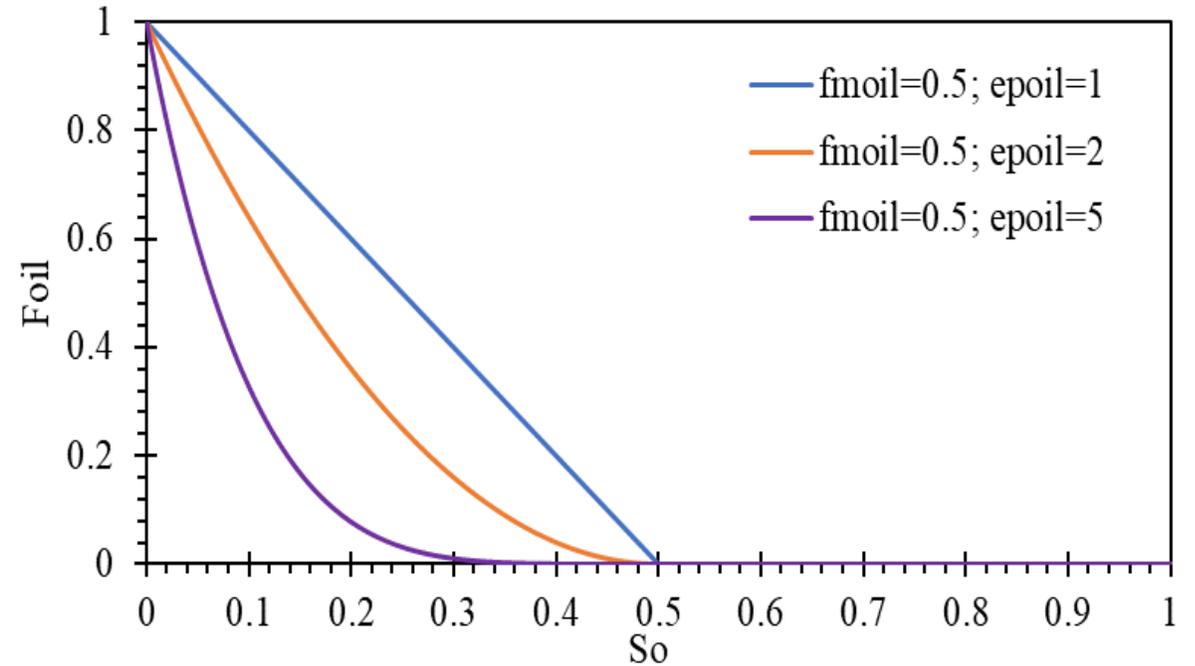
A CO<sub>2</sub> foam quality with 1 wt% TTM scan without oil and with 3% crude oil present, in an Indiana limestone core

# Parameters in oil saturation dependent function: $f_{moil}$ & $e_{poil}$

Oil saturation dependence function: Effect of  $f_{moil}$



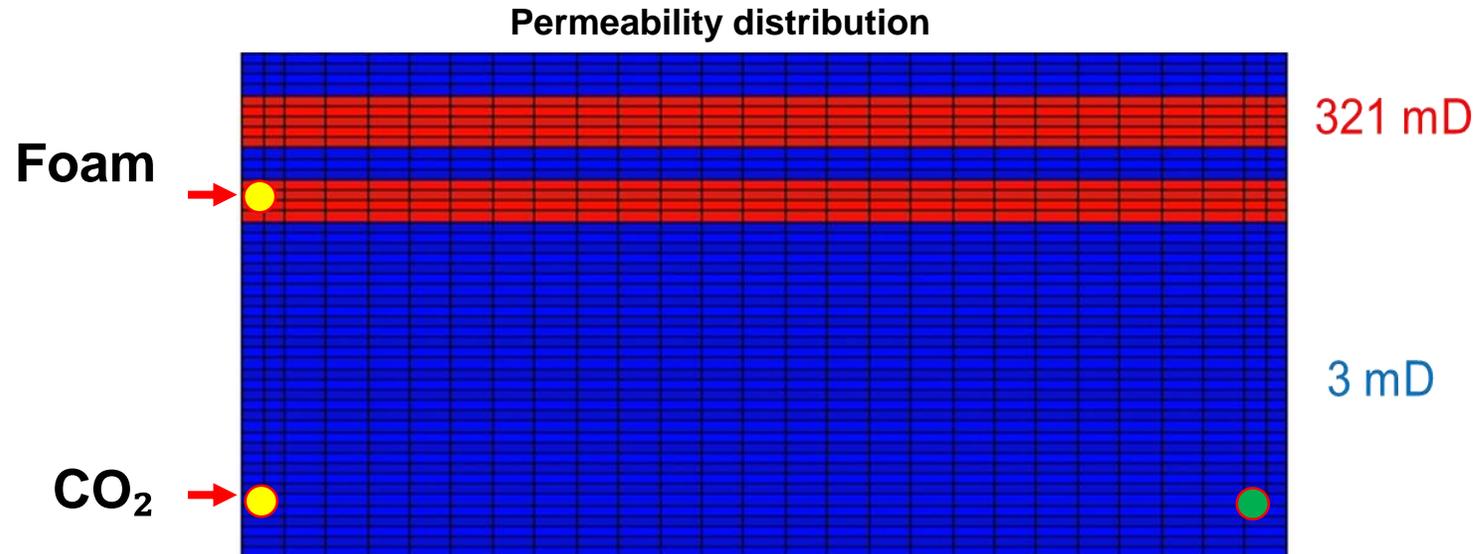
Oil saturation dependence function: Effect of  $e_{poil}$



<p><b>Oil saturation</b></p>	$F_{oil} = \begin{cases} 0 & \text{for } S_o > f_{moil} \\ \left( \frac{f_{moil} - S_o}{f_{msurf} - f_{loil}} \right)^{e_{poil}} & \text{for } f_{loil} < S_o < f_{moil} \\ 1 & \text{for } S_o < f_{loil} \end{cases}$	<p>for <math>S_o &gt; f_{moil}</math> for <math>f_{loil} &lt; S_o &lt; f_{moil}</math> for <math>S_o &lt; f_{loil}</math></p>
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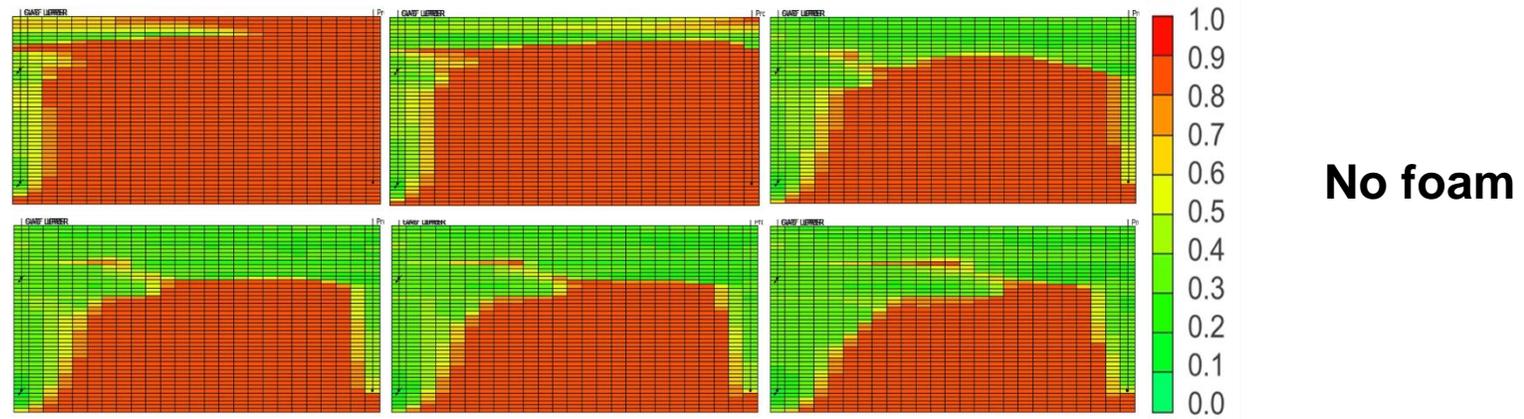
# Heterogeneous reservoir model

## Foam simulation at reservoir scale

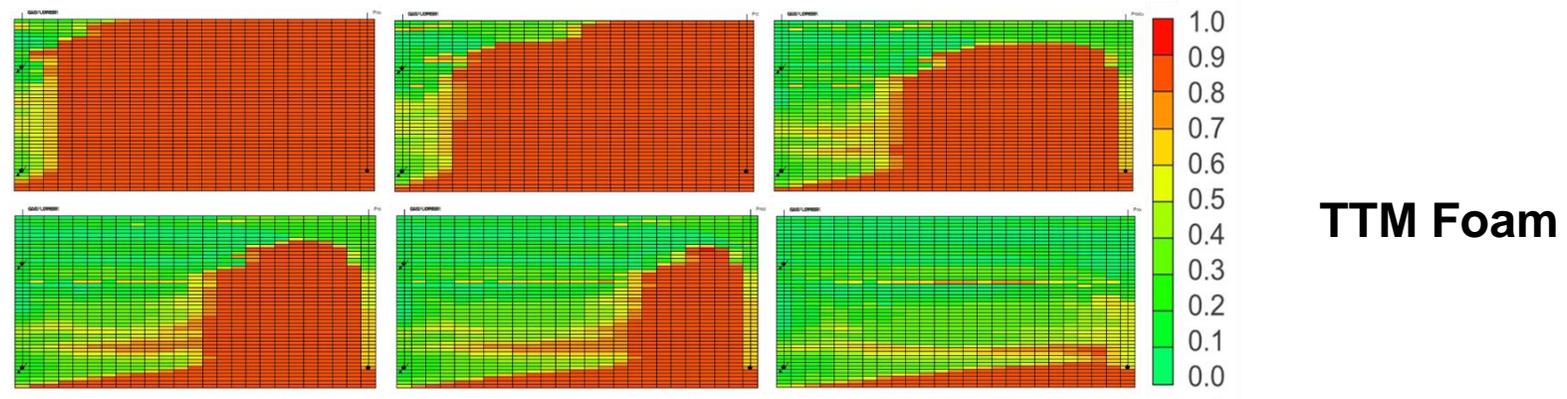


- A **heterogeneous model reservoir** is used
- Top layer permeability 321 mD
- Bottom layer permeability 3 mD
- STARS parameters from **TTM foam test in a 321mD Indianan limestone**
- Injected foam quality  $f_g=0.8$

# Foam simulation at reservoir scale



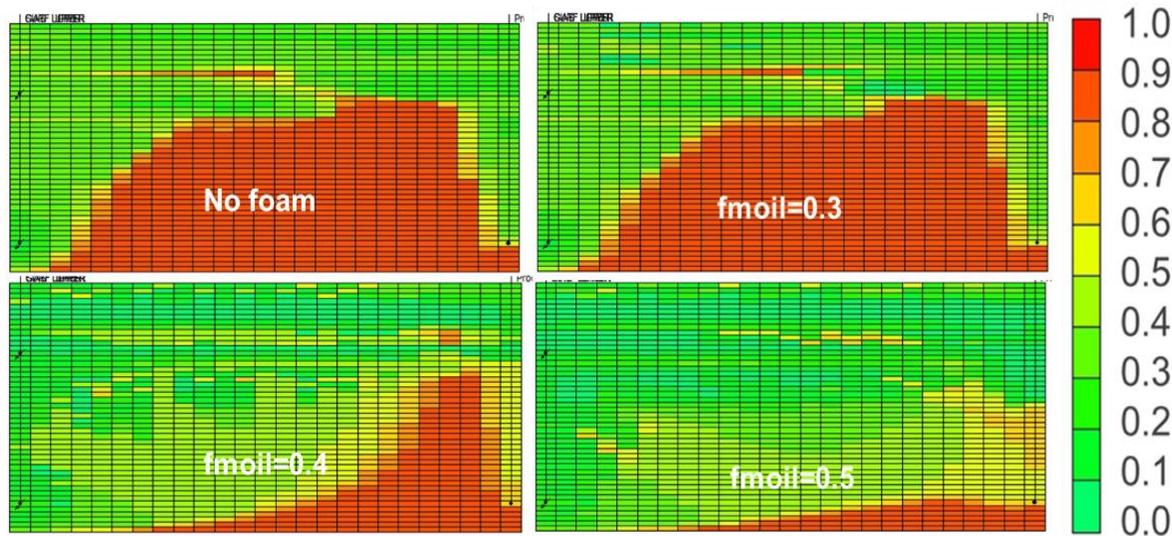
Saturation of oil in the 1<sup>st</sup>, 2<sup>nd</sup>, 5<sup>th</sup>, 8<sup>th</sup>, 10<sup>th</sup>, and 15<sup>th</sup> years with coinjection of brine and CO<sub>2</sub> (80% quality)



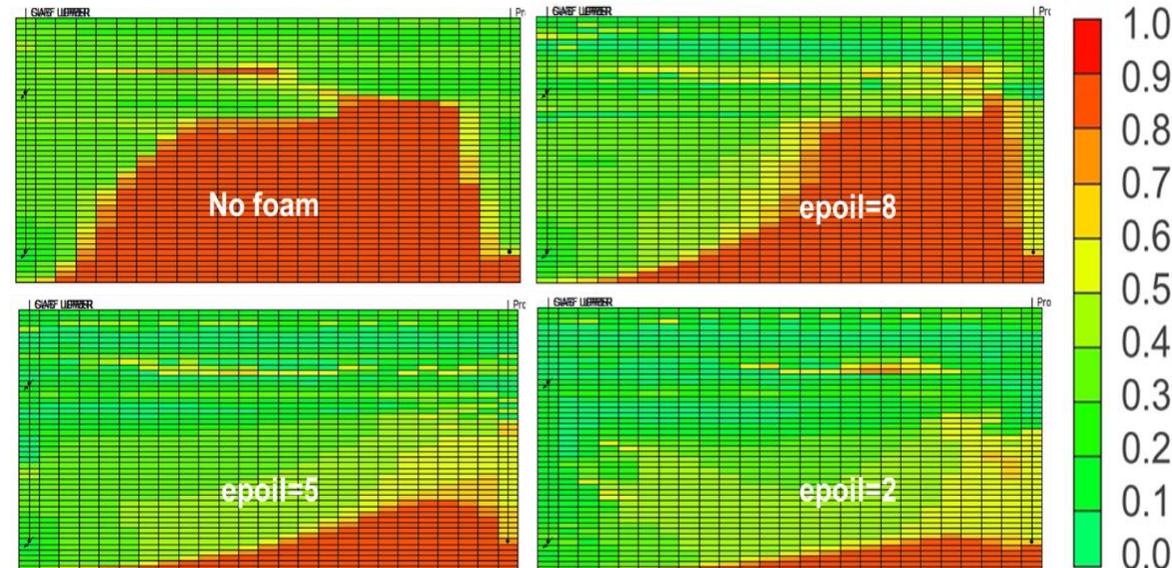
Saturation of oil in the 1<sup>st</sup>, 2<sup>nd</sup>, 5<sup>th</sup>, 8<sup>th</sup>, 10<sup>th</sup>, and 15<sup>th</sup> years with coinjection of TTM and CO<sub>2</sub> (80% quality)

$$f_{moil}=0.5, e_{poil}=1$$

# Effect of oil saturation parameters on foam



Effect of *fmoil* on oil saturation after ~15 yrs of foam flooding at fixed *epoil*=1



Effect of *epoil* on oil saturation after ~15 yrs of foam flooding at fixed *fmoil*=0.5

# Conclusions

- **TTM is stable at high temperature and salinity**
- **Adsorption of TTM on carbonates is low provided that silica and clay contents are low**
- **In the absence of crude oil, TTM does not show MPG for foam generation**
- **TTM foam parameters were obtained, and reservoir simulation shows good mobility control results**
- **Oil saturation parameter plays an important role in the final enhanced oil recovery performance, large  $epoil$  and small  $fmoil$  will reduce the efficiency for TTM foam**

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# References

Jian, G., et al., (2019), "**Evaluating the Transport Behavior of CO<sub>2</sub> Foam in the Presence of Crude Oil under High-Temperature and High-Salinity Conditions for Carbonate Reservoirs,**" *Energy & Fuels*, June, DOI: 10.1021/acs.energyfuels.9b00667.

Zhang, L, et al., (2019), "**Static adsorption of a switchable diamine surfactant on natural and synthetic minerals for high-salinity carbonate reservoirs,**" *Colloids and Surfaces A*. 583, 123910.

Chen, H., Elhag, A. S., Chen, Y., Noguera, J. A., AlSumaiti, A. M., Hirasaki, G. J., Johnston, K. P. (2018). **Oil effect on CO<sub>2</sub> foam stabilized by a switchable amine surfactant at high temperature and high salinity.** *Fuel*, 227, 247–255. <https://doi.org/10.1016/j.fuel.2018.04.020>

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