

**NORTEX 2017**

**Enhancing Carbon Dioxide  
Enhanced Oil Recovery**

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# **Outline of Presentation**

- **West Texas Carbonates**
- **Middle East Reservoirs**
  - **Reservoir conditions**
  - **Surfactants**
  - **Solubility in brine and CO<sub>2</sub>**
  - **Dependence on salinity and temperature**
  - **Adsorption**
- **Conclusions**

# **Nonionic surfactant for low-temperature West Texas carbonate formation**

- **Silurian Core Sample**
- **Diameter=1.5 in.**
- **Length= 7.6 cm= 2.99 in.**
- **Permeability= 48.9 md**
- **L24-22: alcohol (22 EO) with linear hydrophobe (C12-14) from Huntsman, the activity of solution is 1(wt)% /DI (assume the activity is 100%).**

# Flooding Condition

- Pressure= **3400 psi**
- Temperature=room temperature, **~25 °C**
- Flooding Speed: **4 ft/day**
- Injection Schemes: Co-injection, WAG or SAG and 100% CO<sub>2</sub> continuous injection

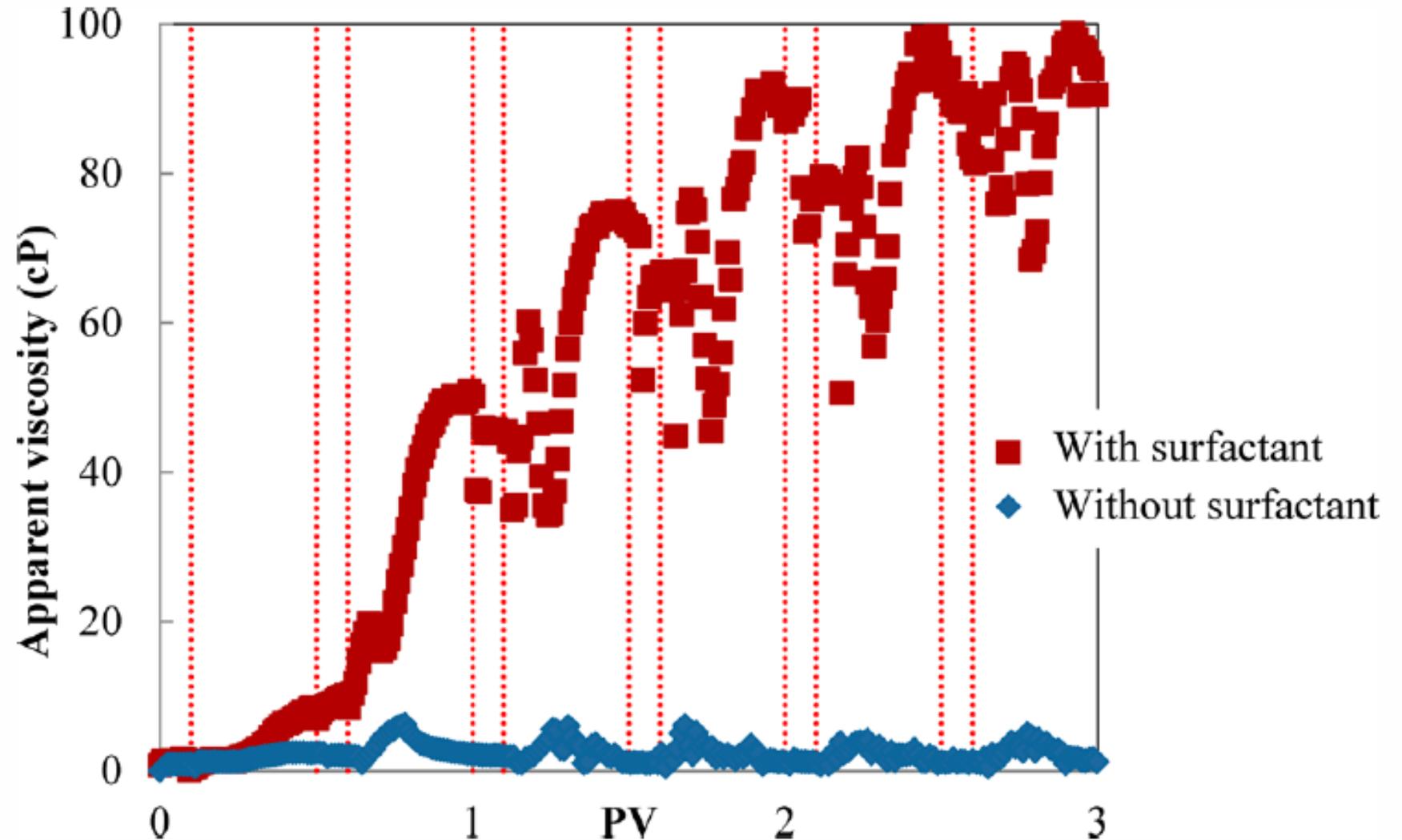
# Pressure Gradient Expressed as Apparent Viscosity

- Apparent viscosity is used to describe the foam strength, which is calculated by Darcy's law:

$$\mu_{app} = - \frac{k \nabla p}{(u_w + u_{CO_2})}$$

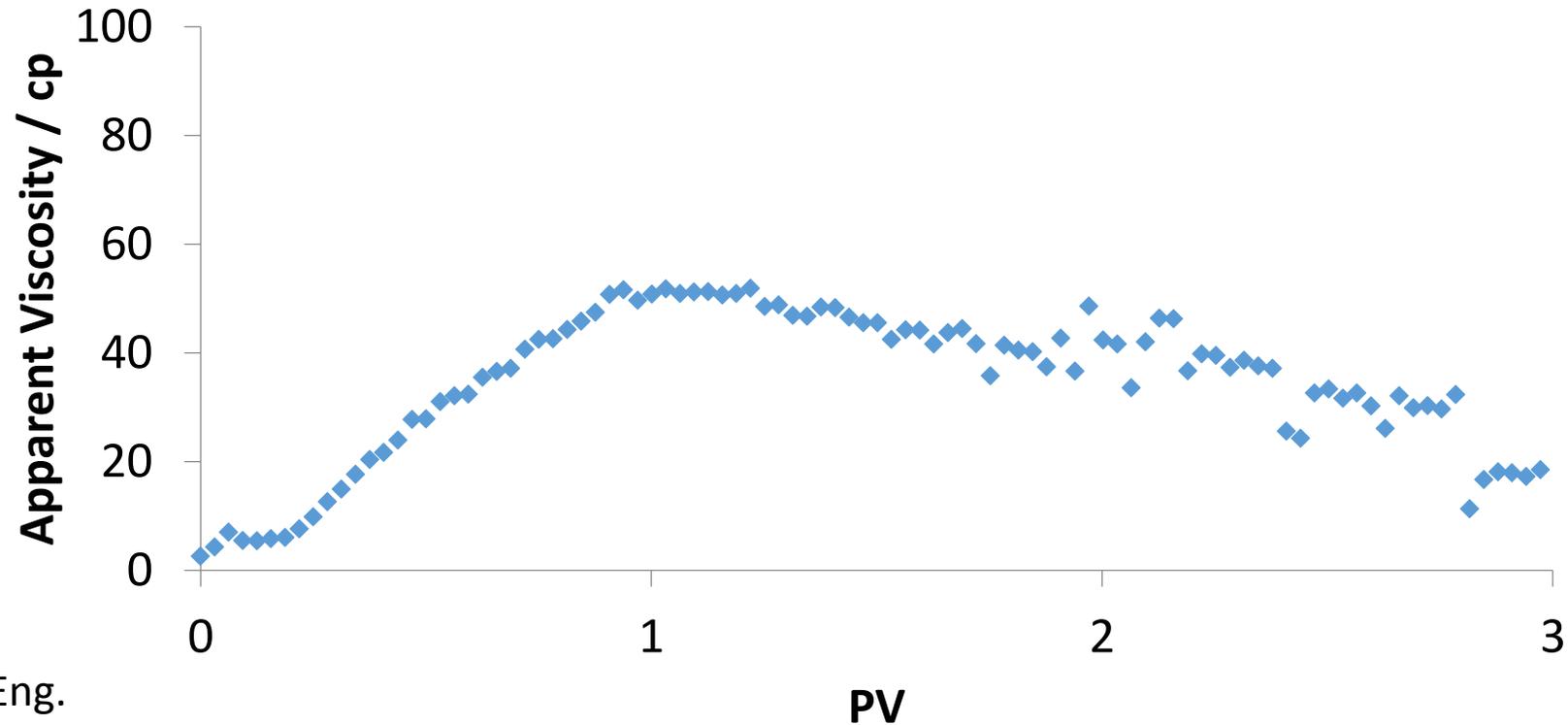
where  $\mu_{app}$  is foam apparent viscosity,  $k$  is core permeability,  $u$  is the total superficial velocity and  $p$  is the pressure gradient.

# SAG, 80% CO<sub>2</sub> and 20% L24-22 /DI (1wt%), at 4 ft/day



Chen, et al., 2015, Ind. Eng. Chem. Res., 54, 4252-4263.

# Continuous 100% CO<sub>2</sub> Injection , at 4 ft/day



Chen, et al., 2015, Ind. Eng.  
Chem. Res., 54, 4252-4263.

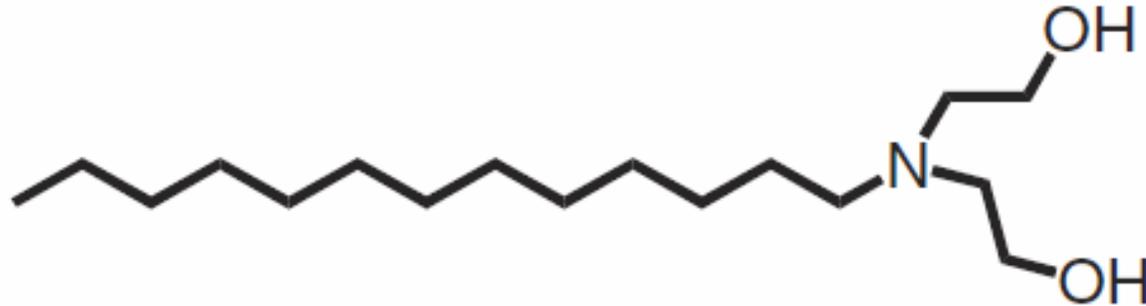
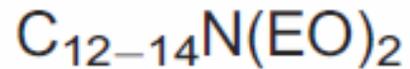
**4 PV of L24-22/DI (1wt%) solution are injected into core at 4 ft/day, before inject CO<sub>2</sub>**

# Middle East Flooding Conditions

- **Temperature=120 °C**
- **Pressure = 3,400 psi**
- **Salinity = 22% TDS**
- **Carbonate Formation**

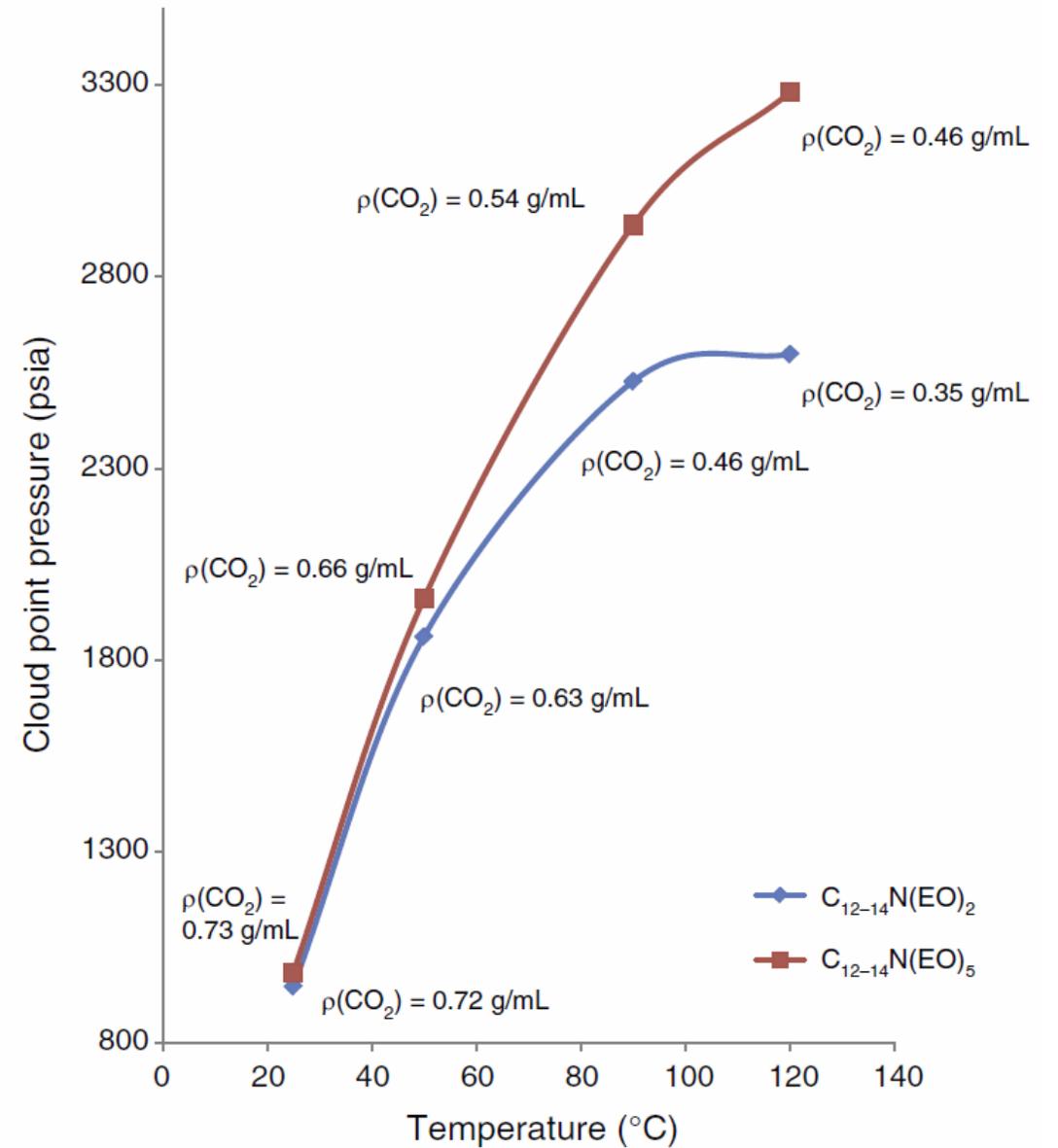
# Surfactant for High Temperature, High Salinity, Carbonate Reservoirs

Ethomeen C/12



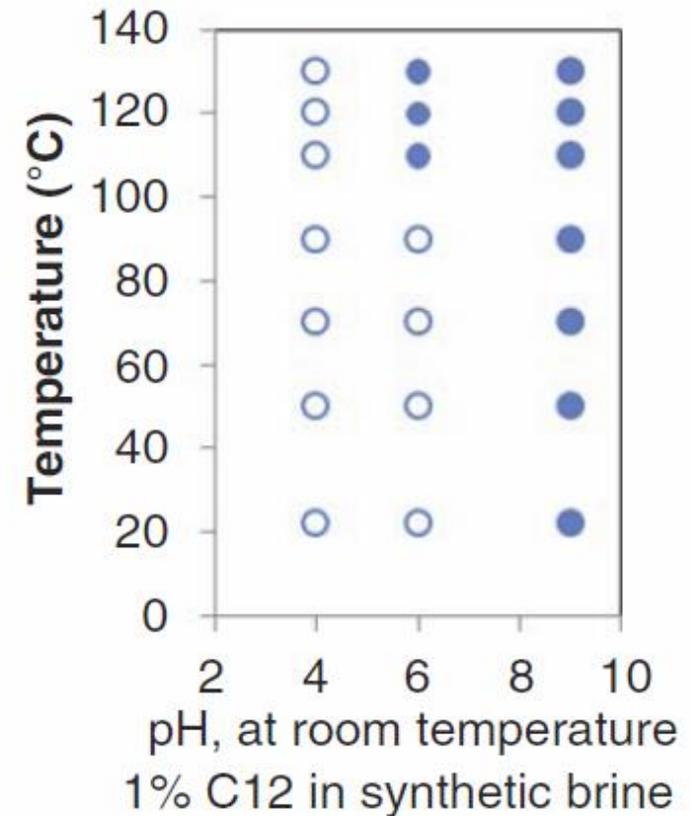
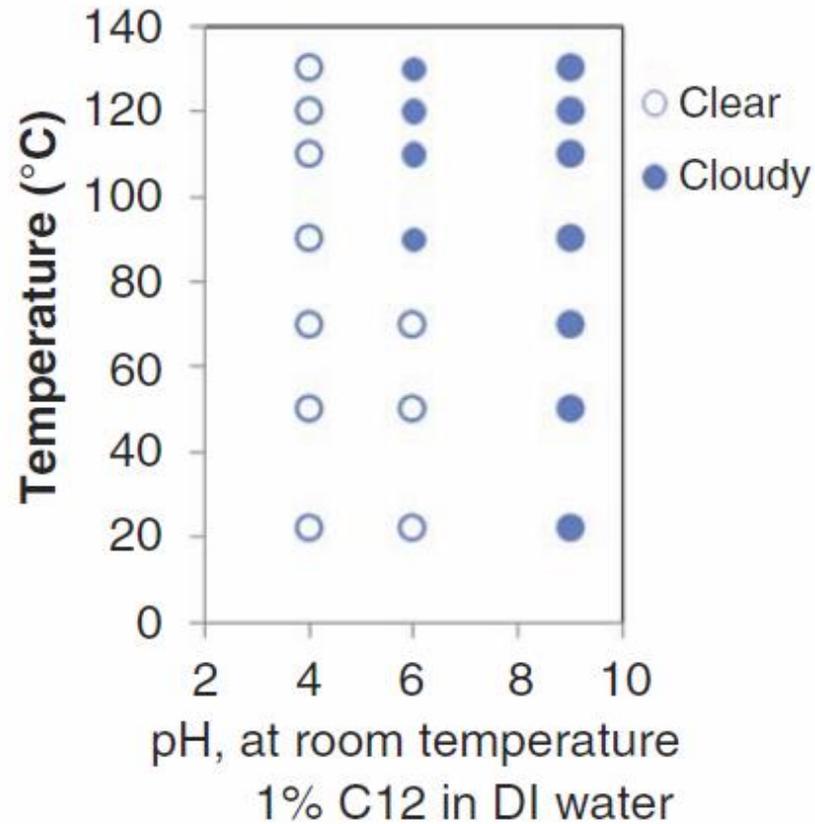
Hydroxyl groups added hydrophilicity  
Raised solubility in water

# Surfactant can be dissolved in CO<sub>2</sub>

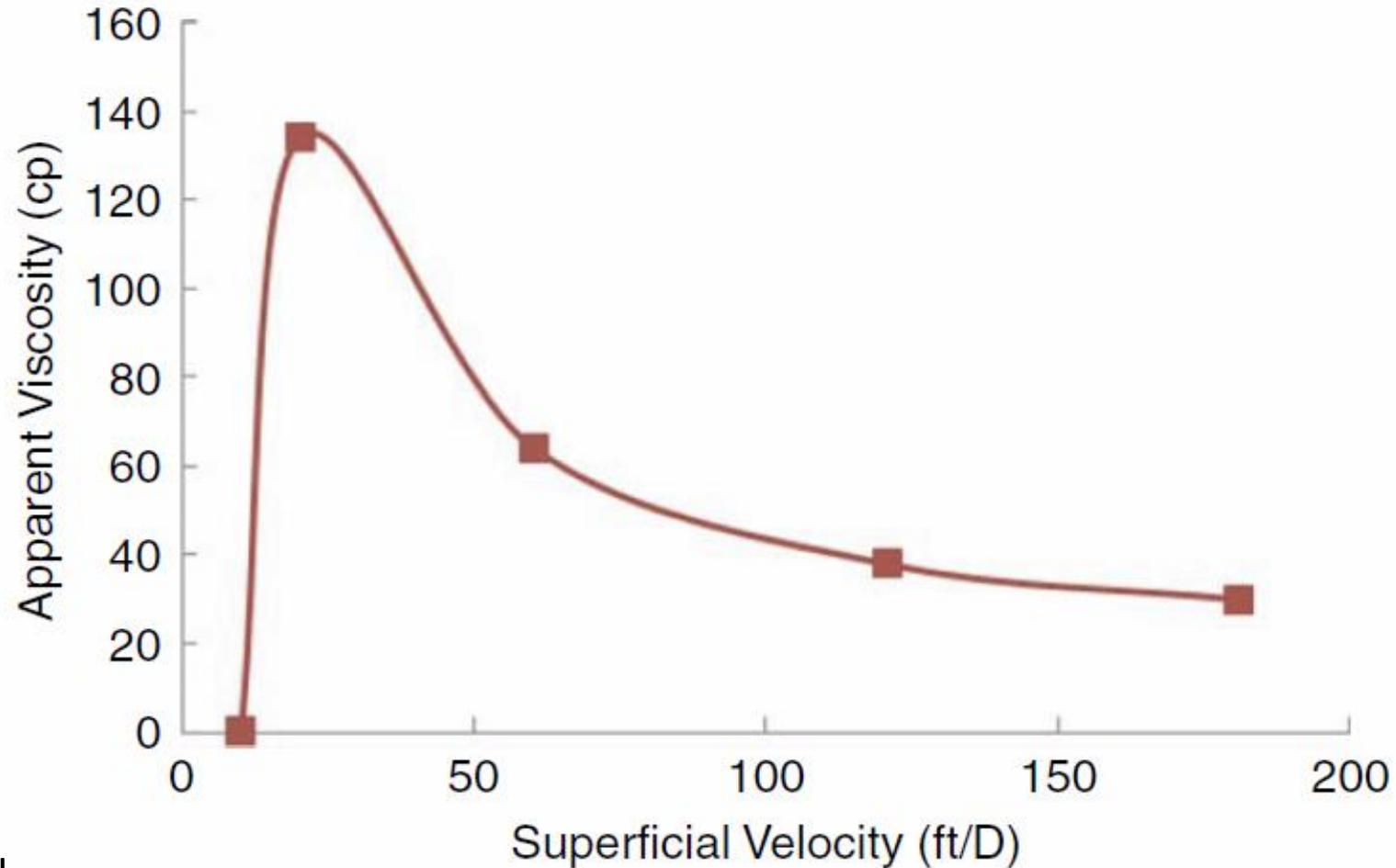


# Surfactant is Soluble in Water or Brine at Low pH

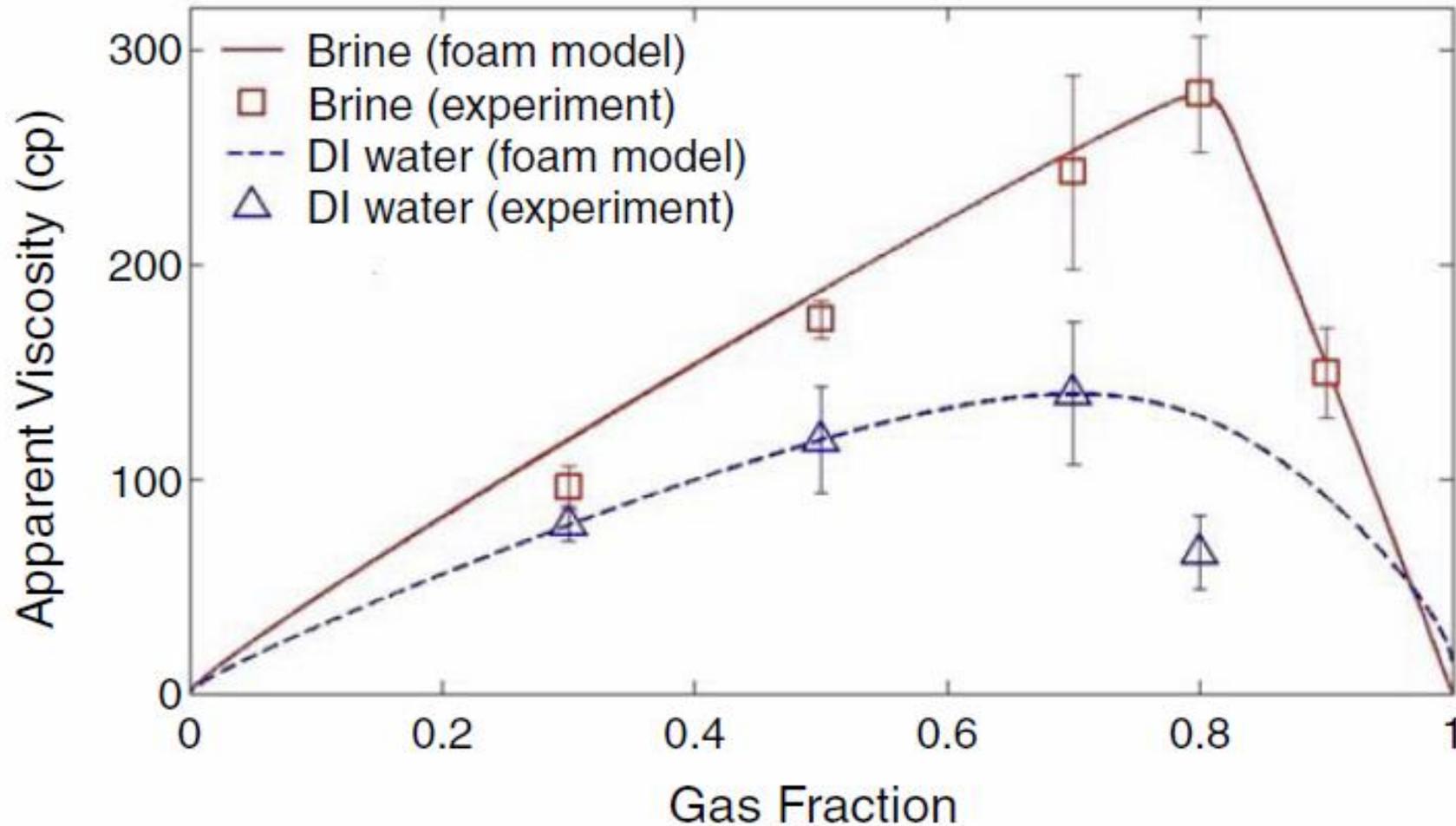
Brine in Equilibrium with CO<sub>2</sub> at High Pressure is pH 4



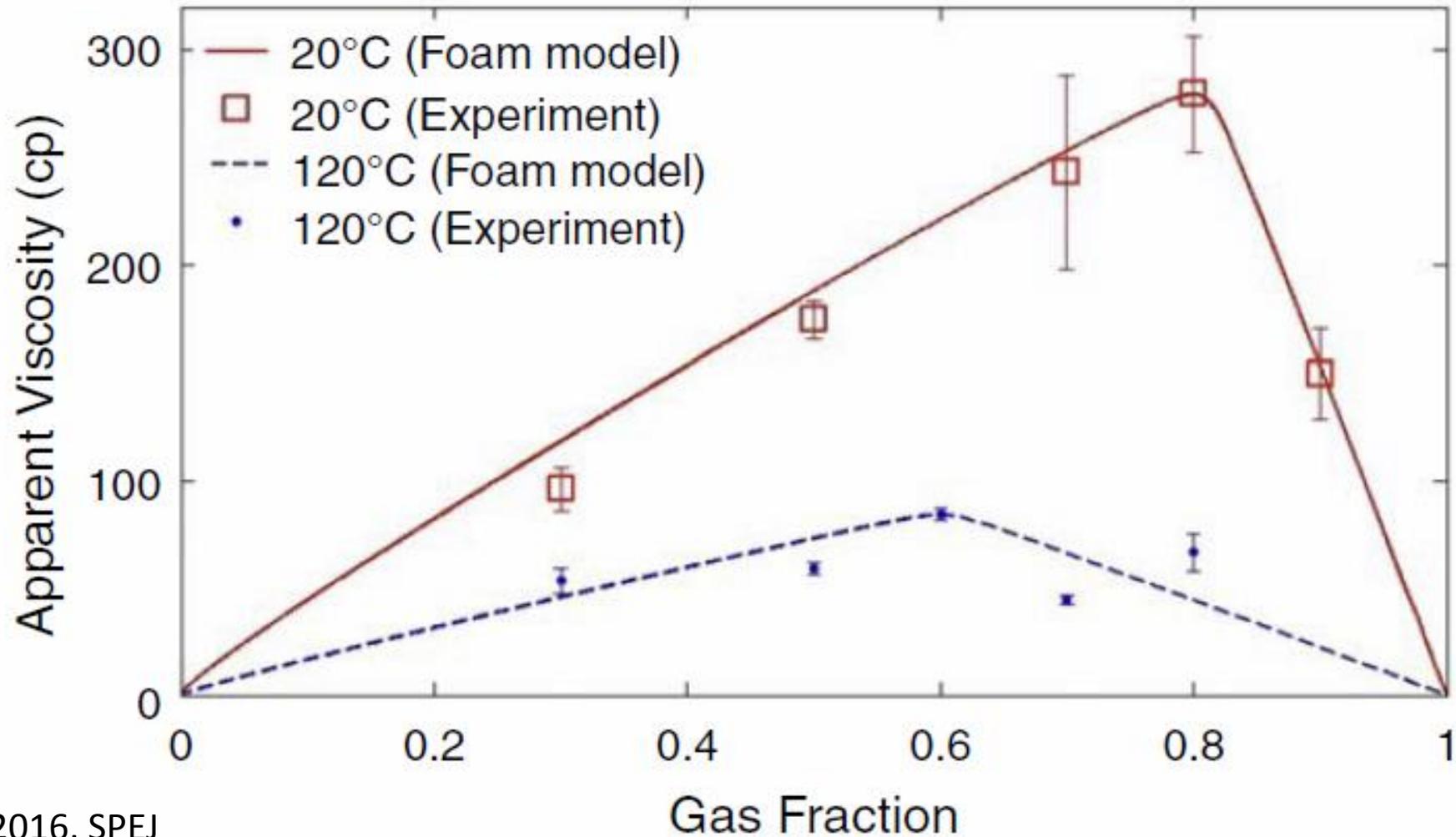
# Minimum Pressure Gradient is Needed to Generate Foam In Situ; Then Shear-Thinning



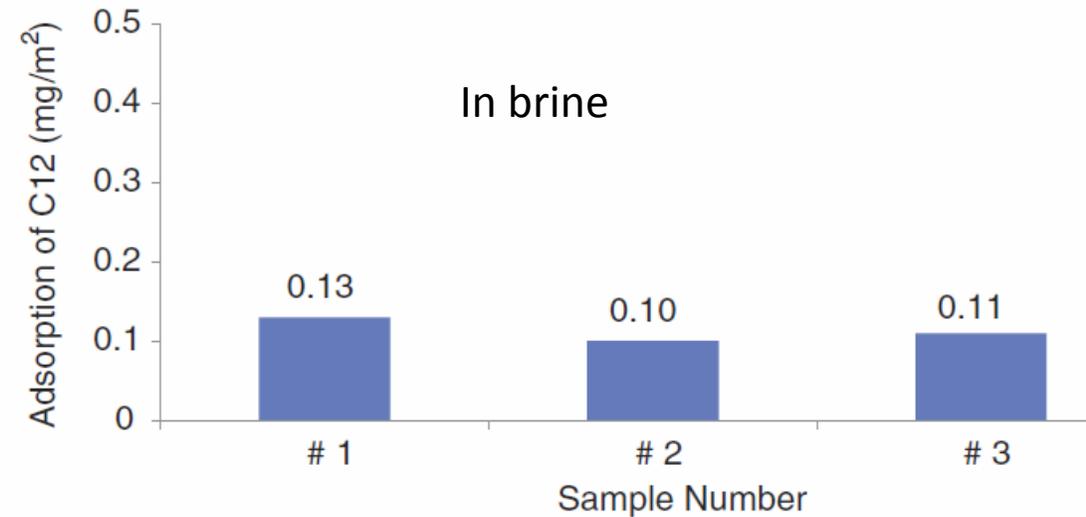
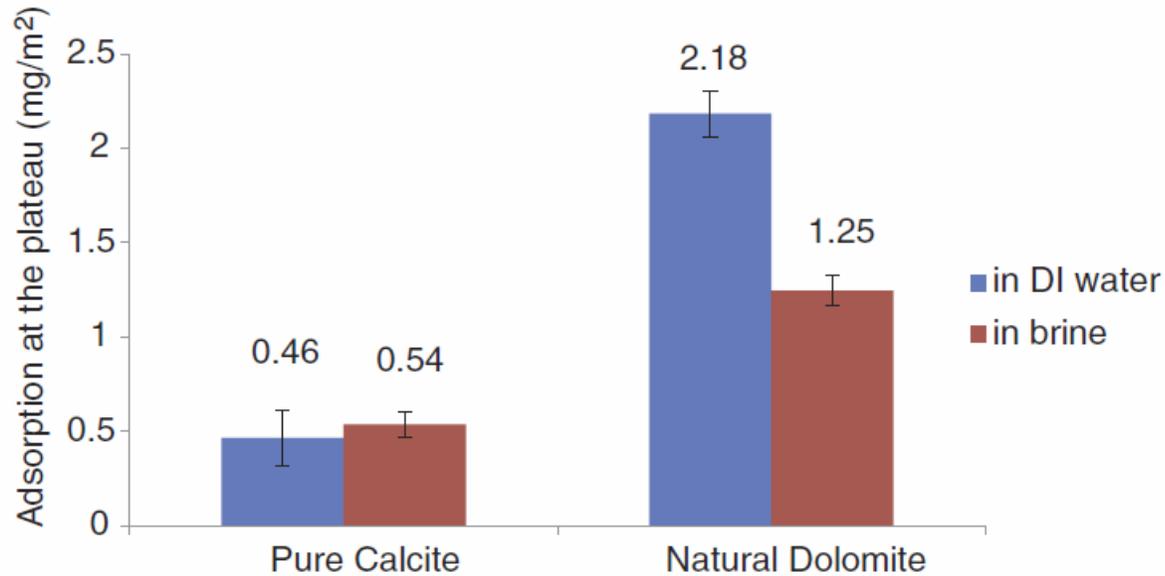
# Effect of 22% TDS Brine on Foam Strength Room Temperature



# Effect of Reservoir Temperature on Foam Strength 22% TDS Brine



# Adsorption of C/12 on Carbonate Rocks



**Formation Material**

BET area= 4.0 m<sup>2</sup>/g

# Conclusions

- **CO<sub>2</sub> is available from natural sources and industrial sites**
- **Low viscosity of CO<sub>2</sub> results in poor sweep efficiency**
- **CO<sub>2</sub> can be made viscous by dispersing as foam**
- **Nonionic surfactant is adequate for West Texas**
- **Middle East has high temperature and high salinity**
- **Switchable nonionic to cationic surfactants are candidates for Middle East carbonate reservoirs**